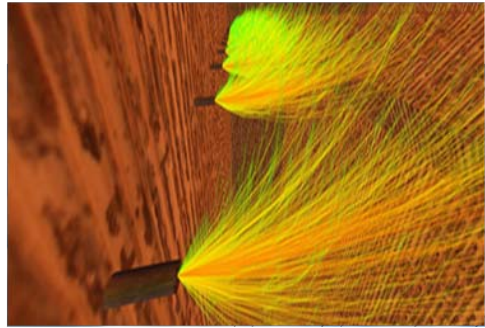


Reinhold Environmental Ltd.



2009 NOx-Combustion Round
Table & Expo Presentation

February 9 & 10, 2009, Cleveland, OH



Targeted-In-Furnace Injection for Slag Control (TIFI)

J.M.Filipski
February 10, 2009

FUEL CHEM[®]

Applications

Coal

- Fuel Chem Programs address slag-forming constituents in a wide range of coals throughout the world

Oil

- High Sulfur Oil
- High slagging oil (Mexico)

Other Fuels

- Biomass
- Pulp and Paper Black Liquor Boilers
- Municipal Solid Waste (TCI[™] Technology)

FUEL CHEM[®] Program

- ❑ Slag – the iron, sodium and other minerals in coal that do not burn
- ❑ Above the ash fusion temperature these minerals melt and adhere to steam pipes and boiler walls
- ❑ More economical coals can have higher slagging properties
- ❑ Traditional removal methods
 - During Operations:
 - Air / water cannons
 - Thermal shocking
 - Shotguns
 - During Outages (6-10 days):
 - Dynamite
 - Mechanical Removal with Scrapers / Chisels / Etc.



Example of a clinker fall

FUEL CHEM[®] Program Benefits

☐ Efficiency

- Recovery of Derated MW
- Heat Rate Improvement for Steam Production
- Reduced Fan Power Requirements
- Reduced Sootblowing
- Reduced Operating O₂ Level
- Reduced CO in Furnace and at the Stack
- Increased Fuel Flexibility

☐ Availability and Reliability

- Reduced Forced Outage Time
- Reduced Derates
- Increased Capacity and Boiler Availability
- Reduced Outage Cleaning Times
- Reduced Exit Gas Temperatures

Additional FUEL CHEM[®] Benefits

Environmental

- **CO₂ Reduction**
- **SO₃ Reduction**
- **Opacity Improvement**
- **Promotes Mercury Capture**
- **Reduced Large Particle (LPA) Ash**

Safety

- **Reduced Maintenance Operations**

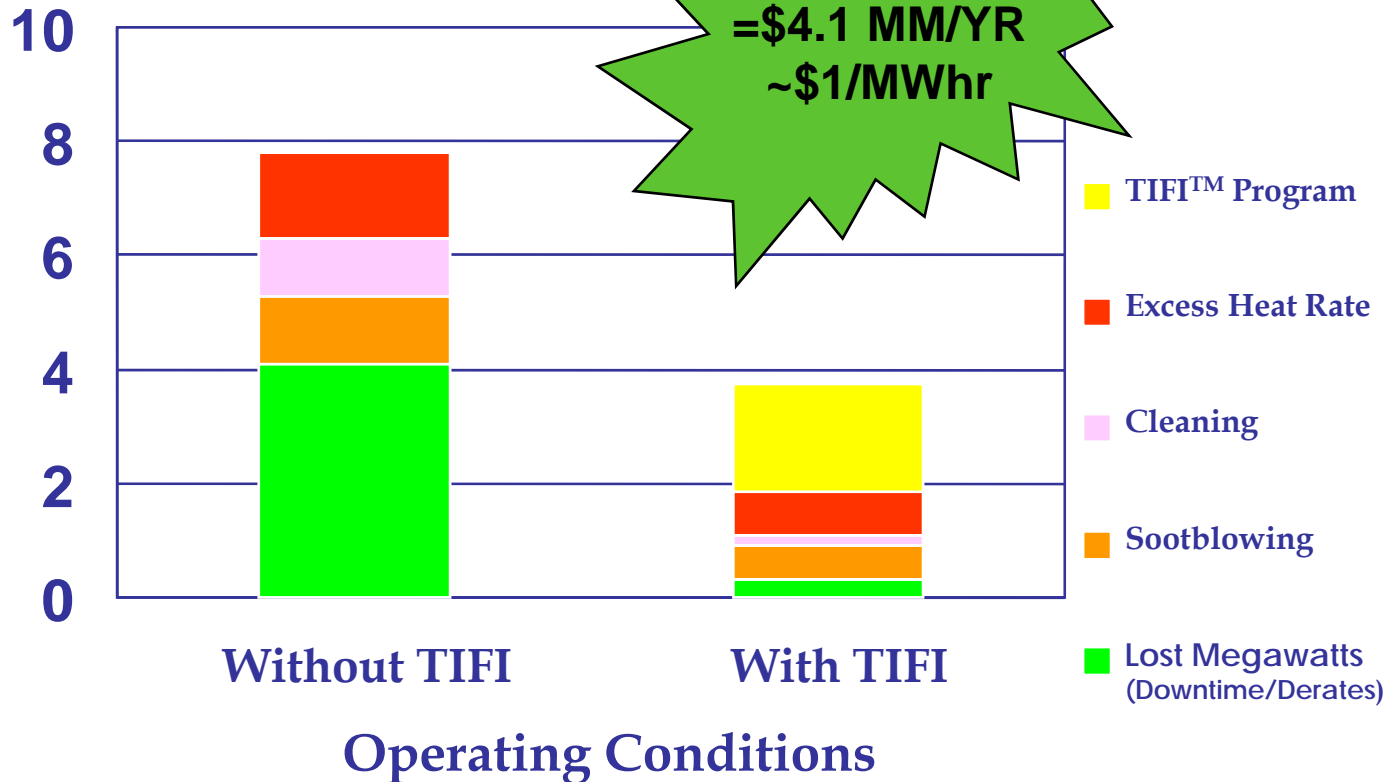
Maintenance

- **Reduced Corrosion in Economizer, Air Heater, Ductwork, and Stack**
- **Reduced Clinker Grinder Maintenance**
- **Tube Life Extension**
 - **Reduced Sootblowing**
 - **Reduced Slag Damage**
- **Reduced Cleaning Expenses**
 - **Less Explosives**
 - **Lower Water Consumption**

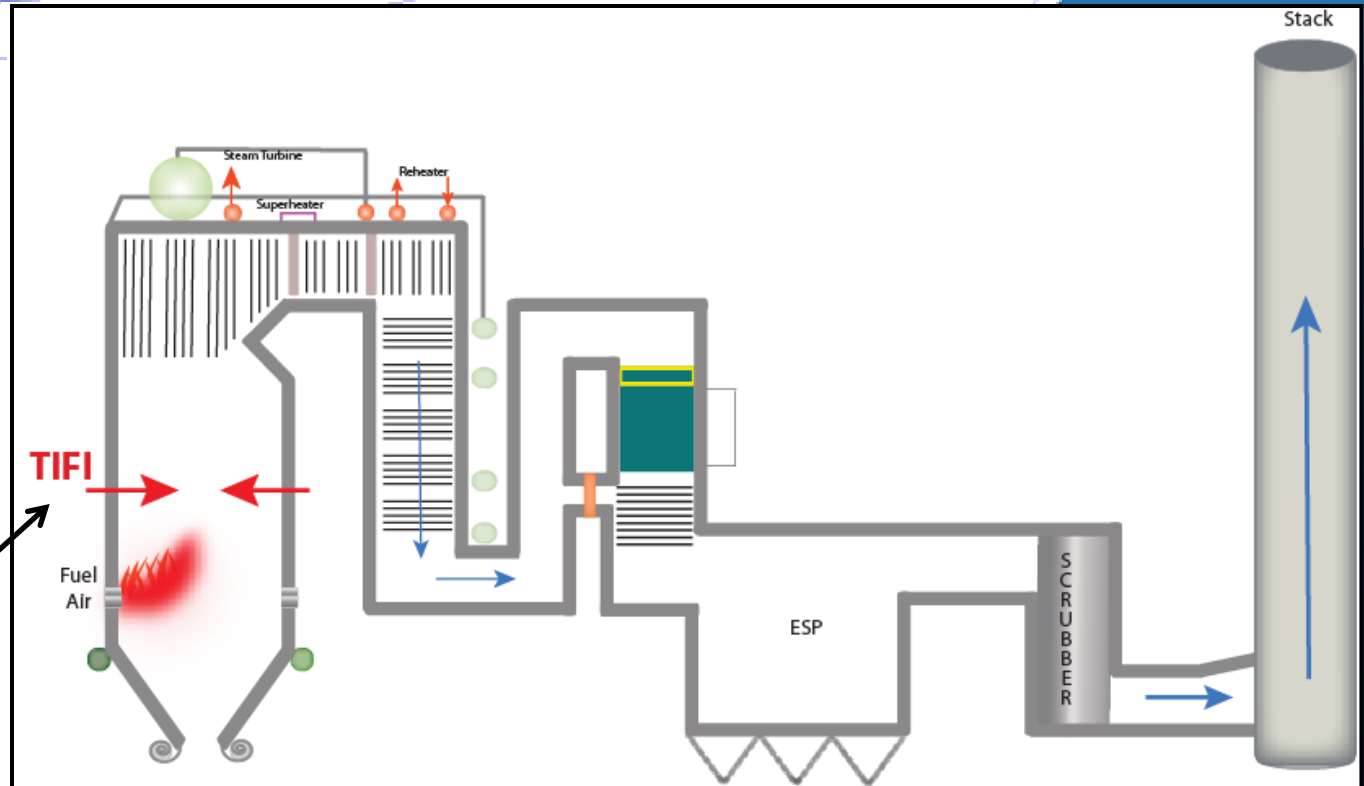
Cost Reduction with TIFI™

Slag Control Budget

500 MW Unit



FUEL CHEM[®] TIFI Overview

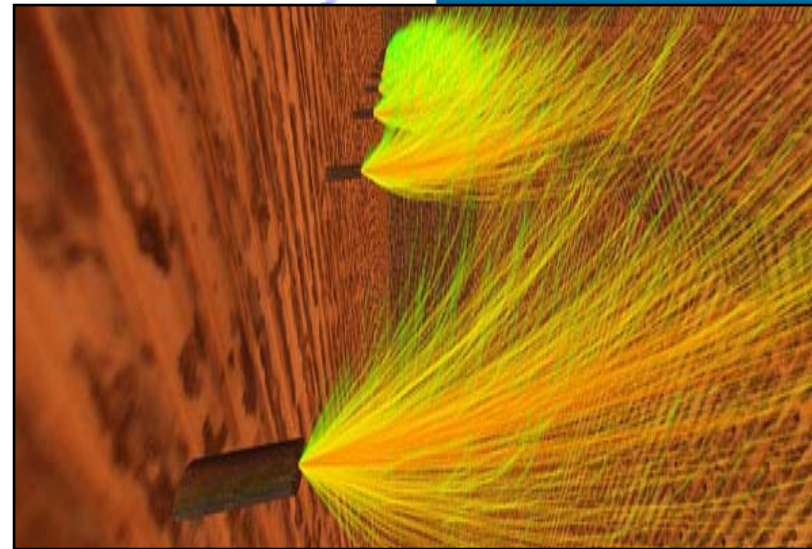


TIFI nozzle injecting Magnesium Hydroxide



TIFI™ Targeted In-Furnace Injection™ Program

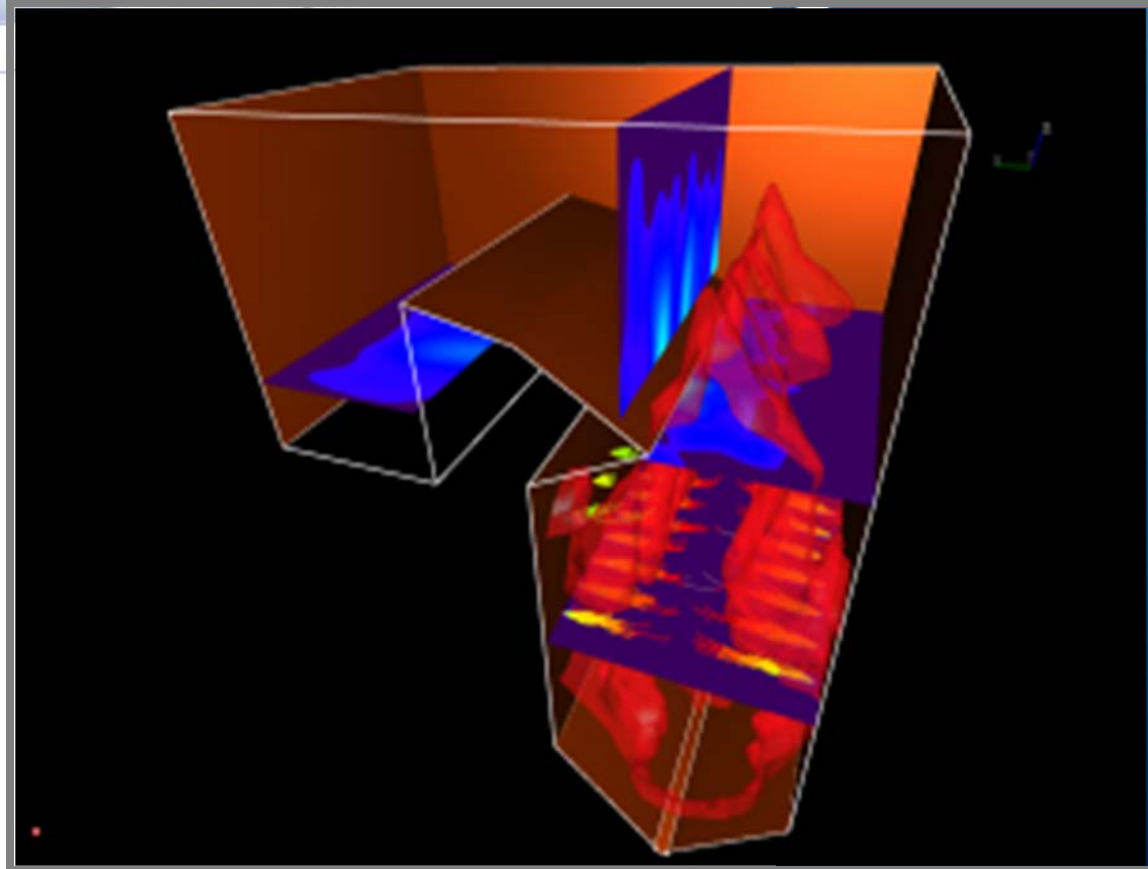
- Patented process for the injection of chemicals using Computational Fluid Dynamic (CFD) modeling as the primary design method
- Critical Criteria
 - Furnace gas flows and temperatures
 - Chemical distribution, particle size and feed rate



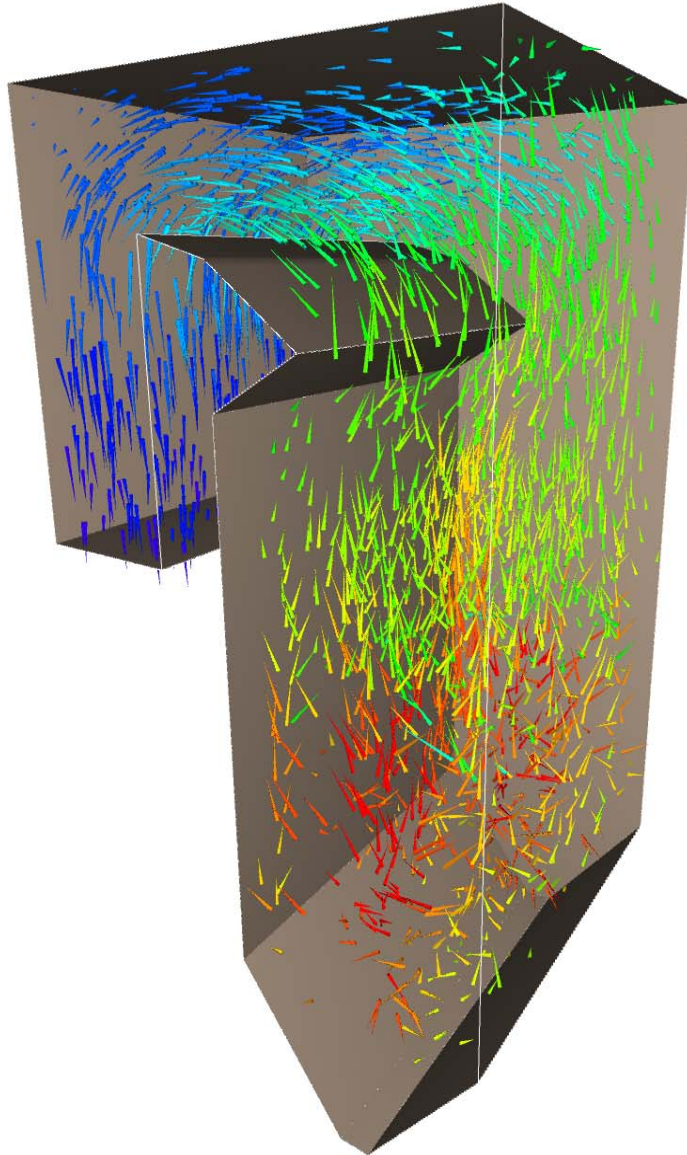
TIFI™ Injector on boiler wall

Computational Fluid Dynamics Modeling

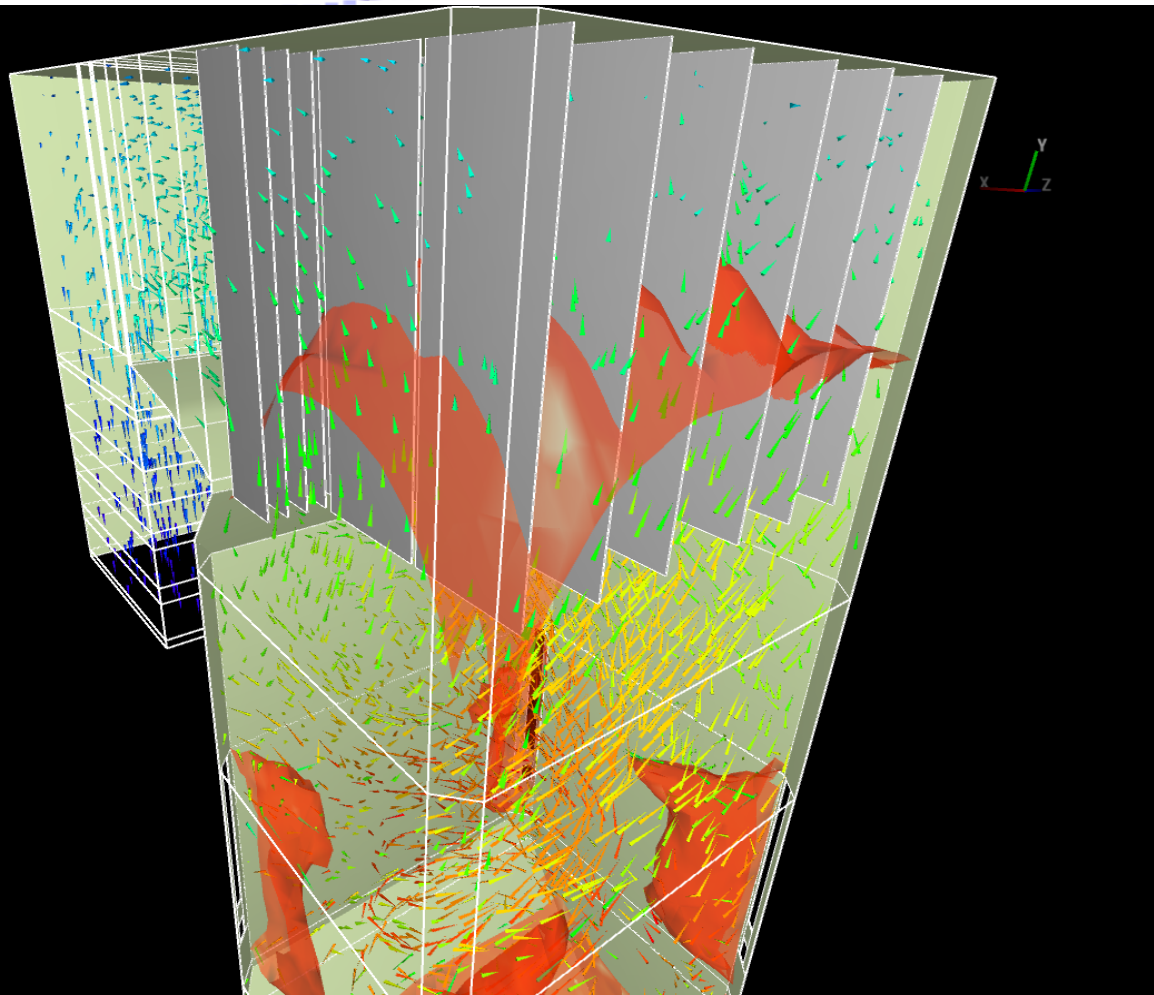
- **Chemical injector sprays (yellow)**
- **Chemical concentration contours (purple and blue)**
- **Temperature isocontours set to the coal ash fusion temperatures to predict potential slagging areas**



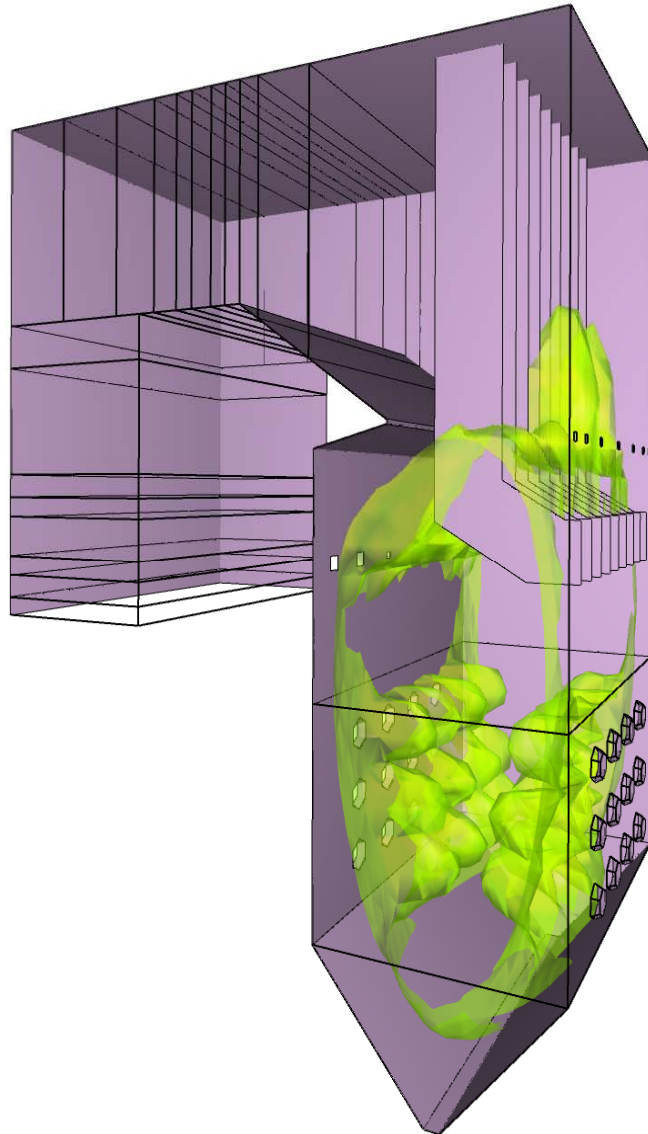
Flue Gas Flow Vectors



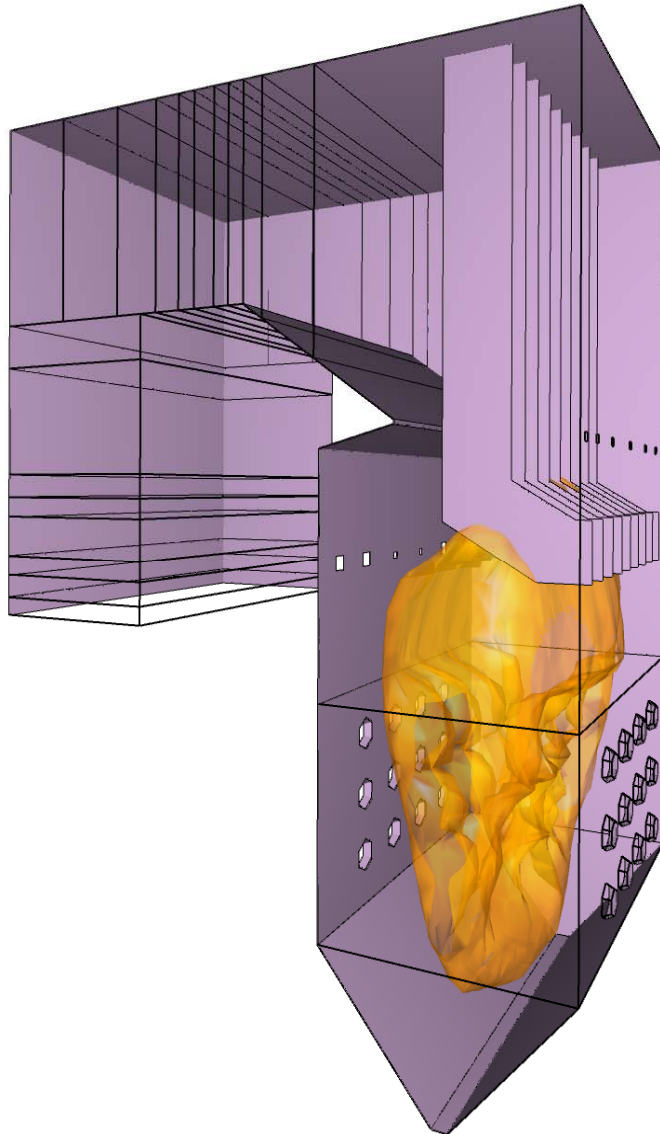
CFD Visualizations of Temperature Surfaces



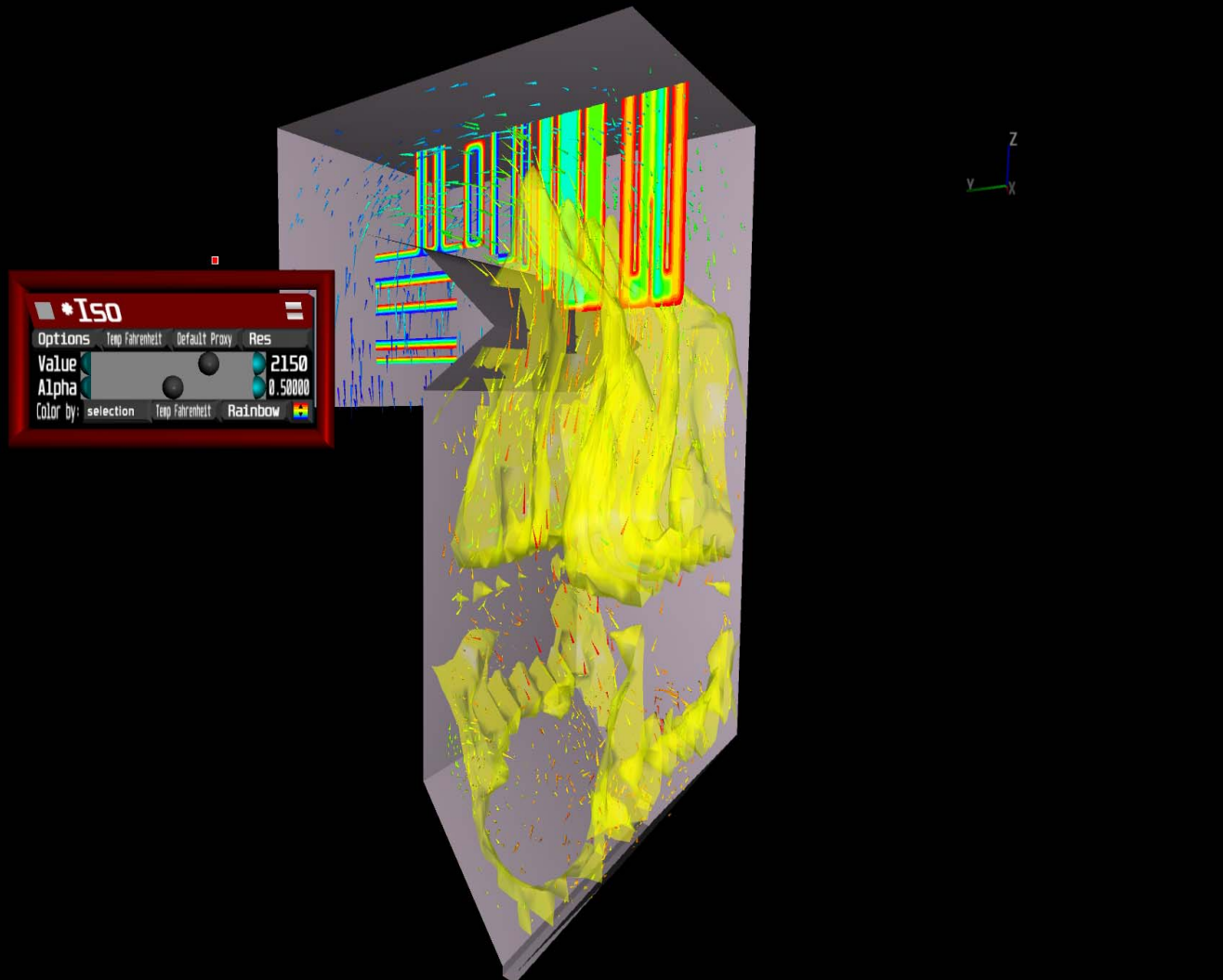
Potential Slagging Areas (Reducing)



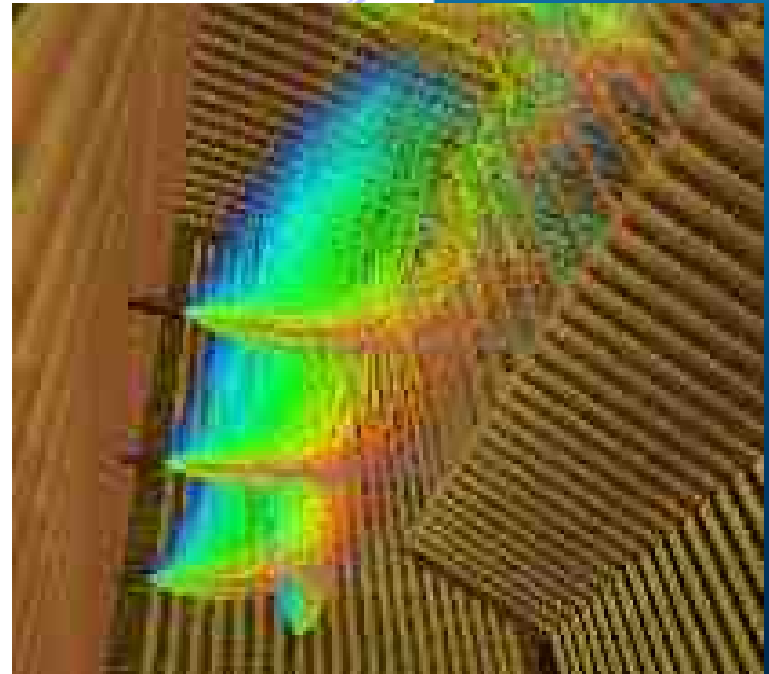
Potential Slagging Areas (Oxidizing)



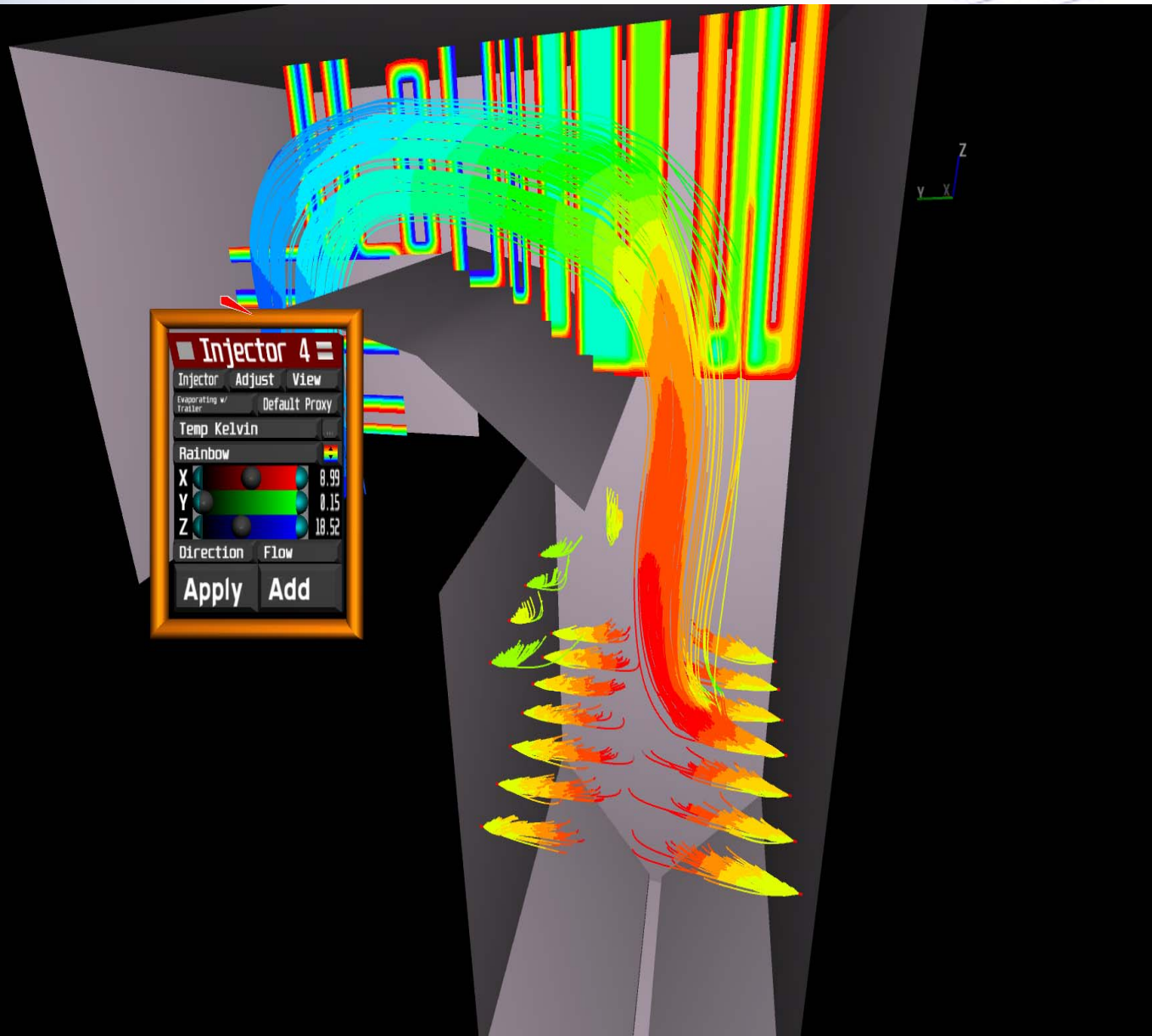
Iso-surface at 2150 F



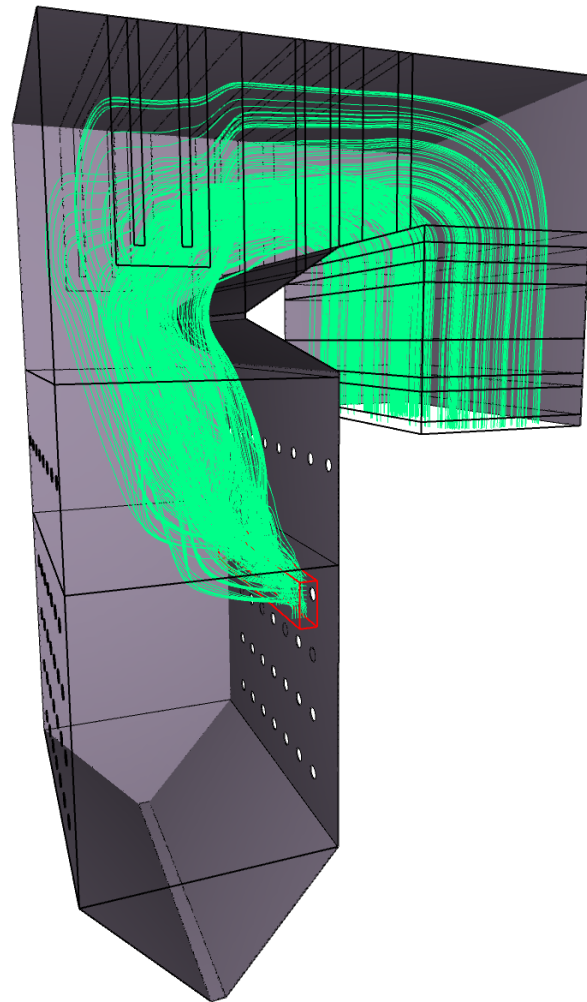
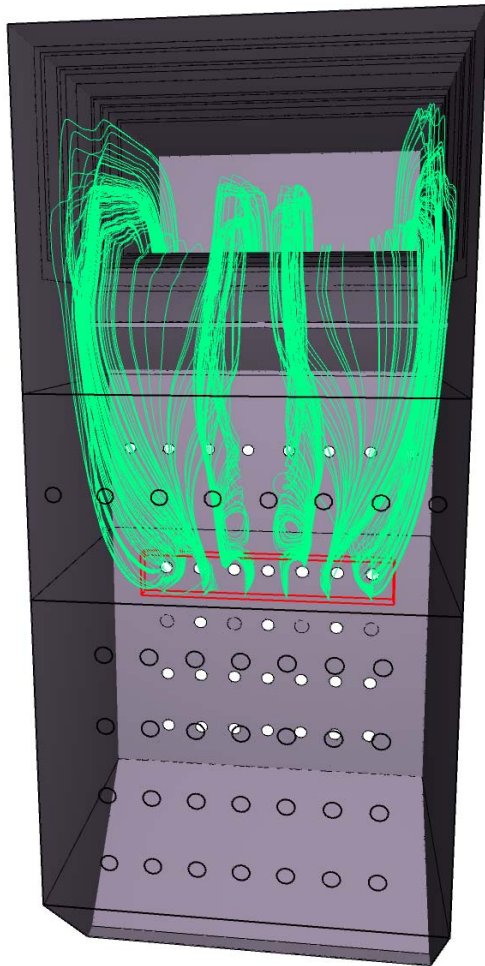
- **Understanding droplet characteristics and trajectories in the boiler environment is critical.**
- **Laser characterization studies of Fuel Chem injectors have been done to accurately predict these droplet characteristics.**



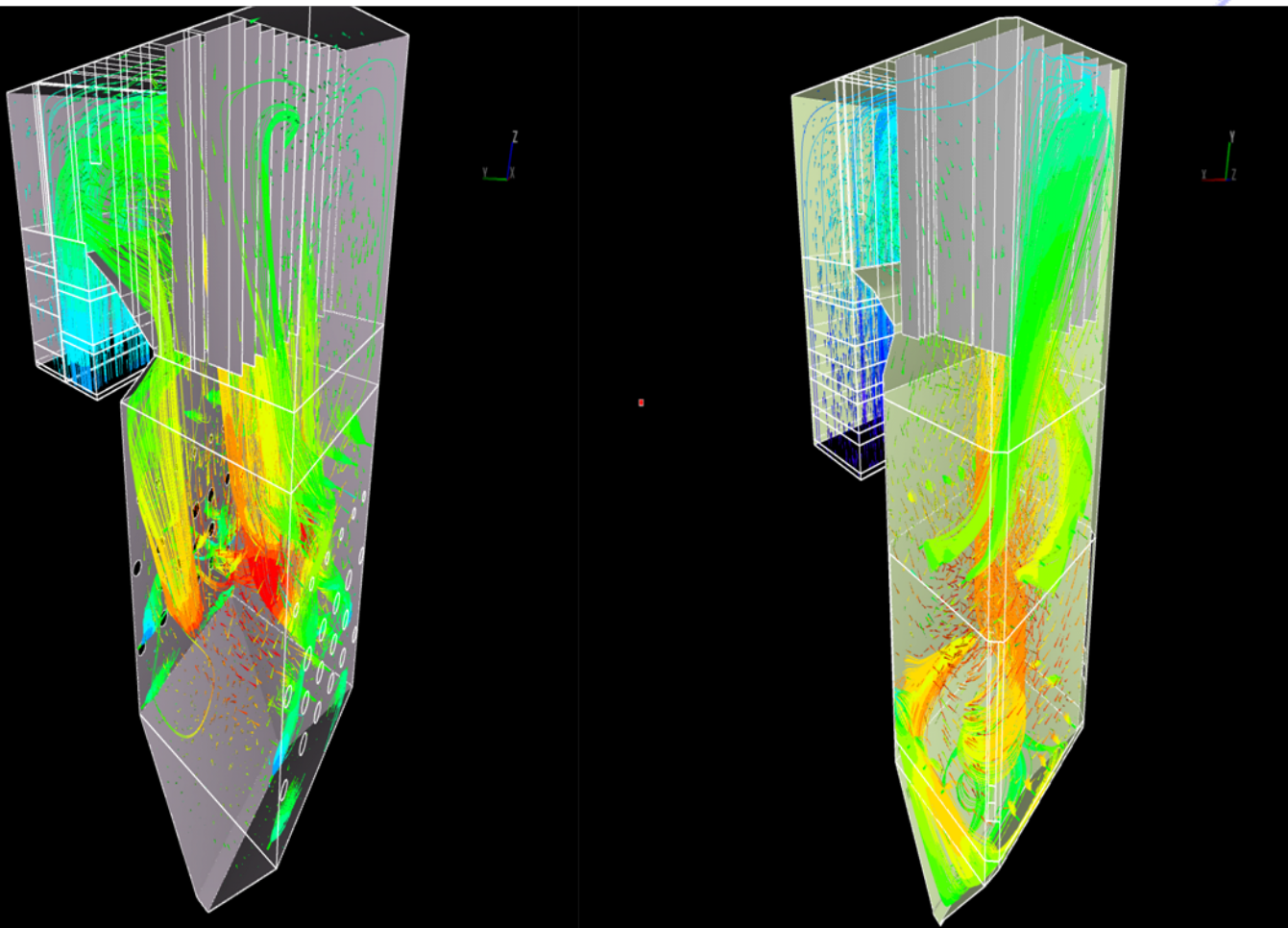
Injector Array with Streamers



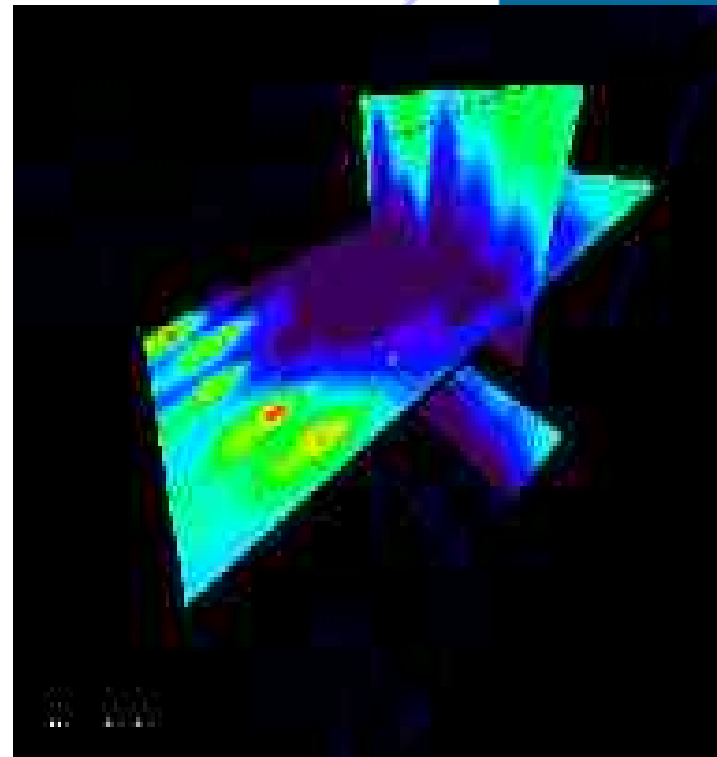
CFD Visualizations of Droplet Trajectories



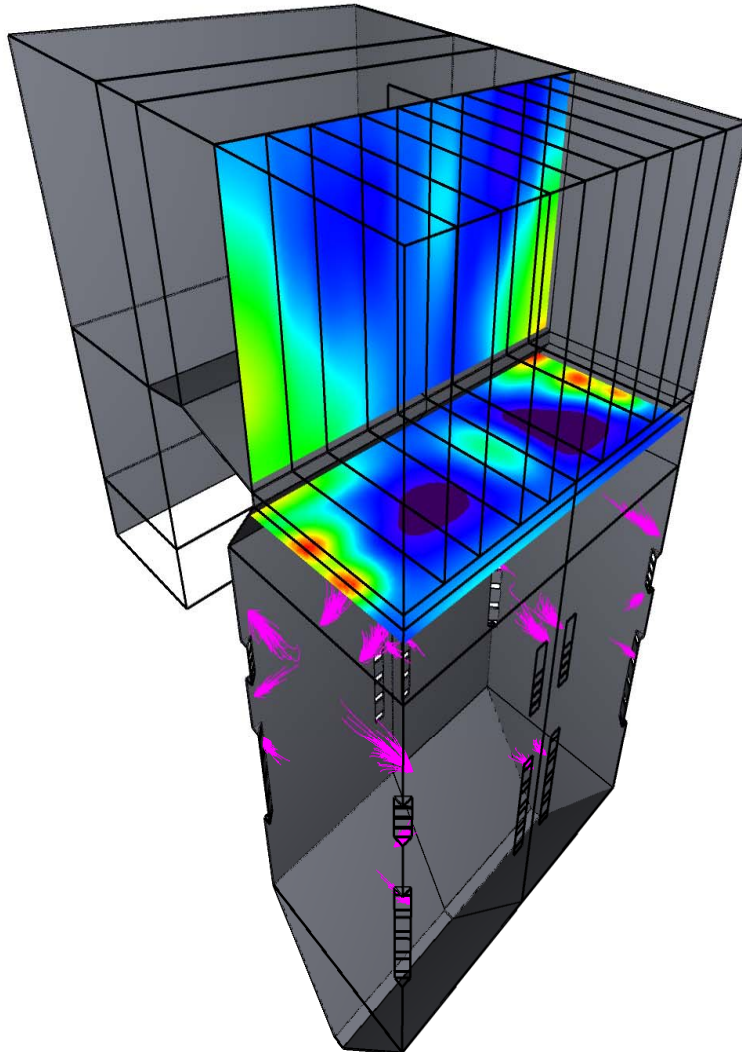
CFD Visualizations of Droplet Trajectories



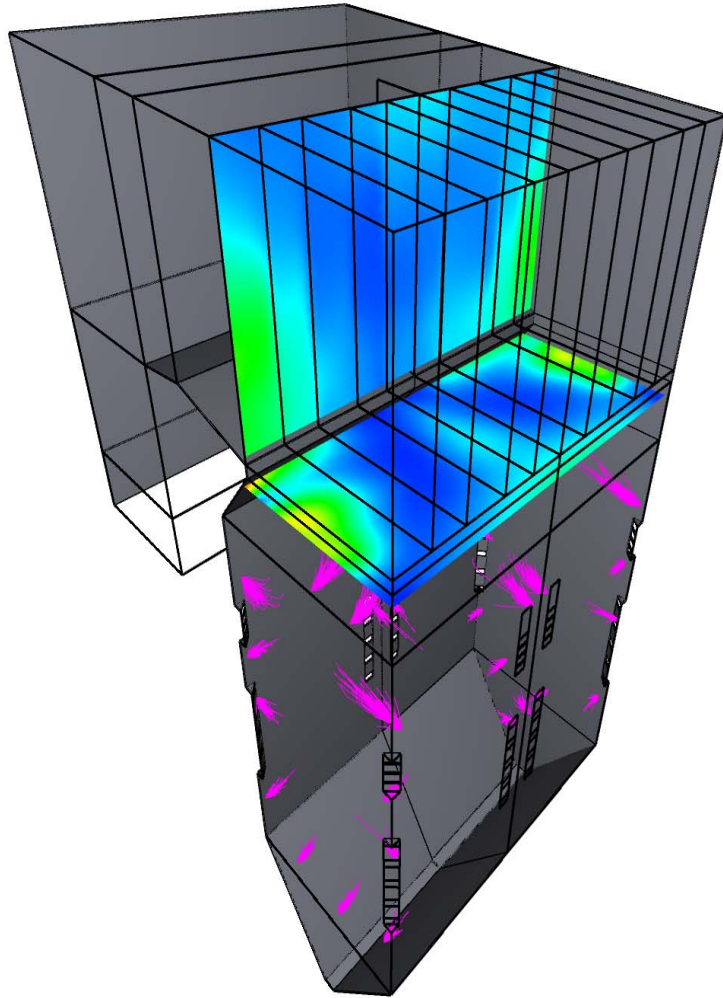
•An injector strategy can now be determined to ensure full coverage by looking at chemical concentrations across several planes.



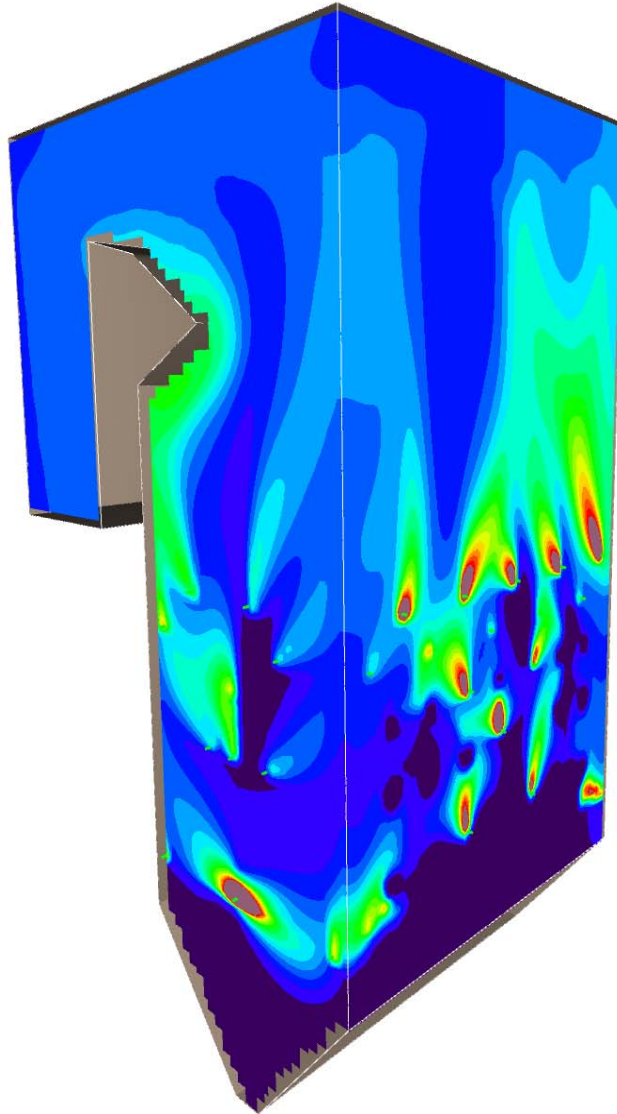
Chemical Coverage Map



Chemical Coverage Map



Front & Left Wall Coverage



MAGNESIUM CHEMISTRIES... NOT IDENTICAL

- *Chemical REACTIVITY*
 - DEAD-, HARD-, LIGHT-Burned MgO
 - Source of MgO; Brine, Mine, Seawater
 - Particle Size, Surface Area and Porosity

Fuel Chem TIFI Process

- **Mg(OH)₂ Injection**

- **Injector Locations**

- Lower and/or upper furnace
- Determined by CFD model for best distribution to problem areas

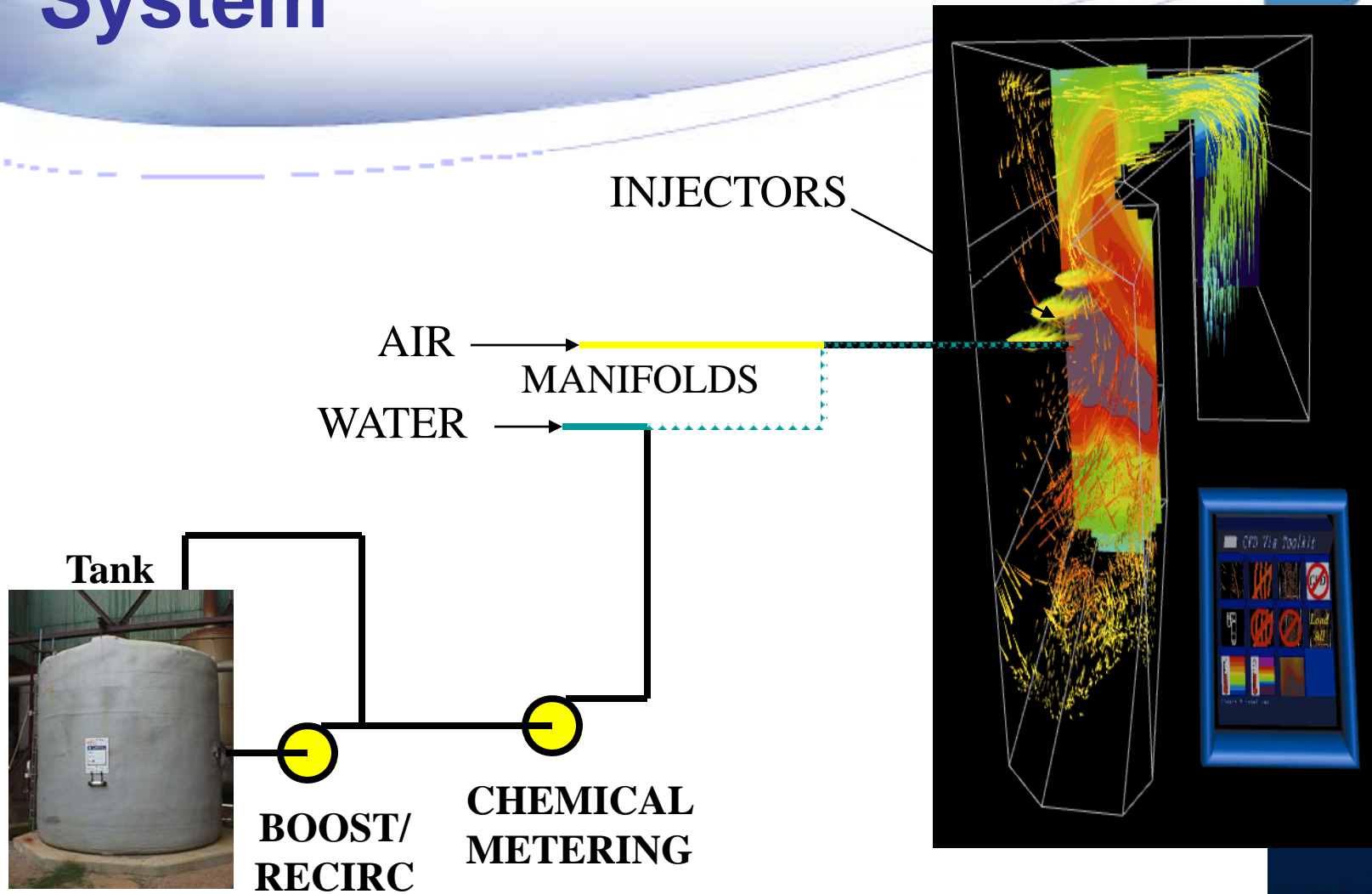
- **Mg(OH)₂ → MgO**
(MP = 5000 F)

- **Reacts with SO₃**
- **Inhibits conversion**

Critical Process Parameters

- Temperature
- O₂
- Soot Blowing
- Mg distribution

Anatomy of a Typical Injection System



Injector Installed and Spraying



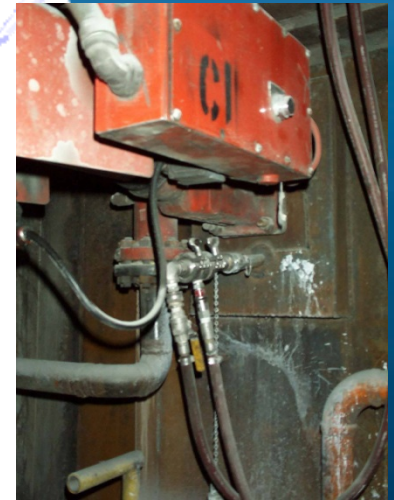
Targeted In Furnace Injectors (TIFI)



DOOR INJECTOR



IR INJECTOR



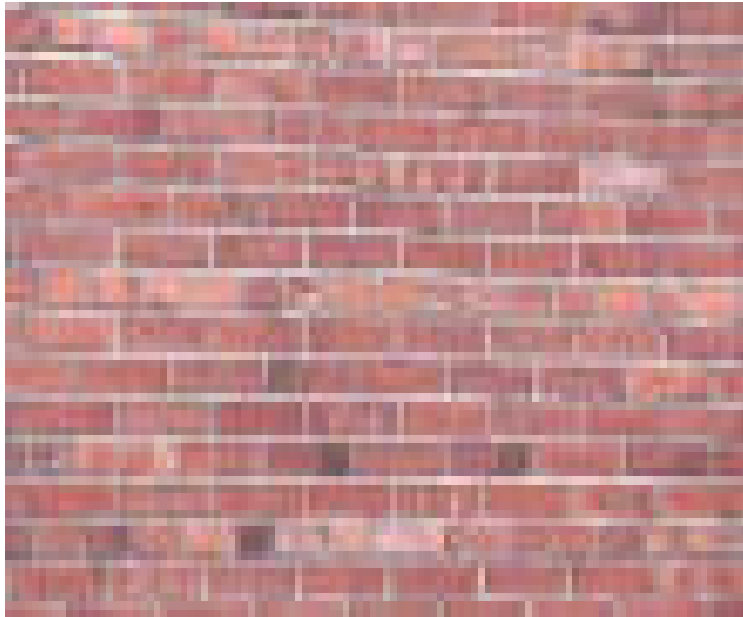
WALL BLOWER INJECTOR

SLAGGING

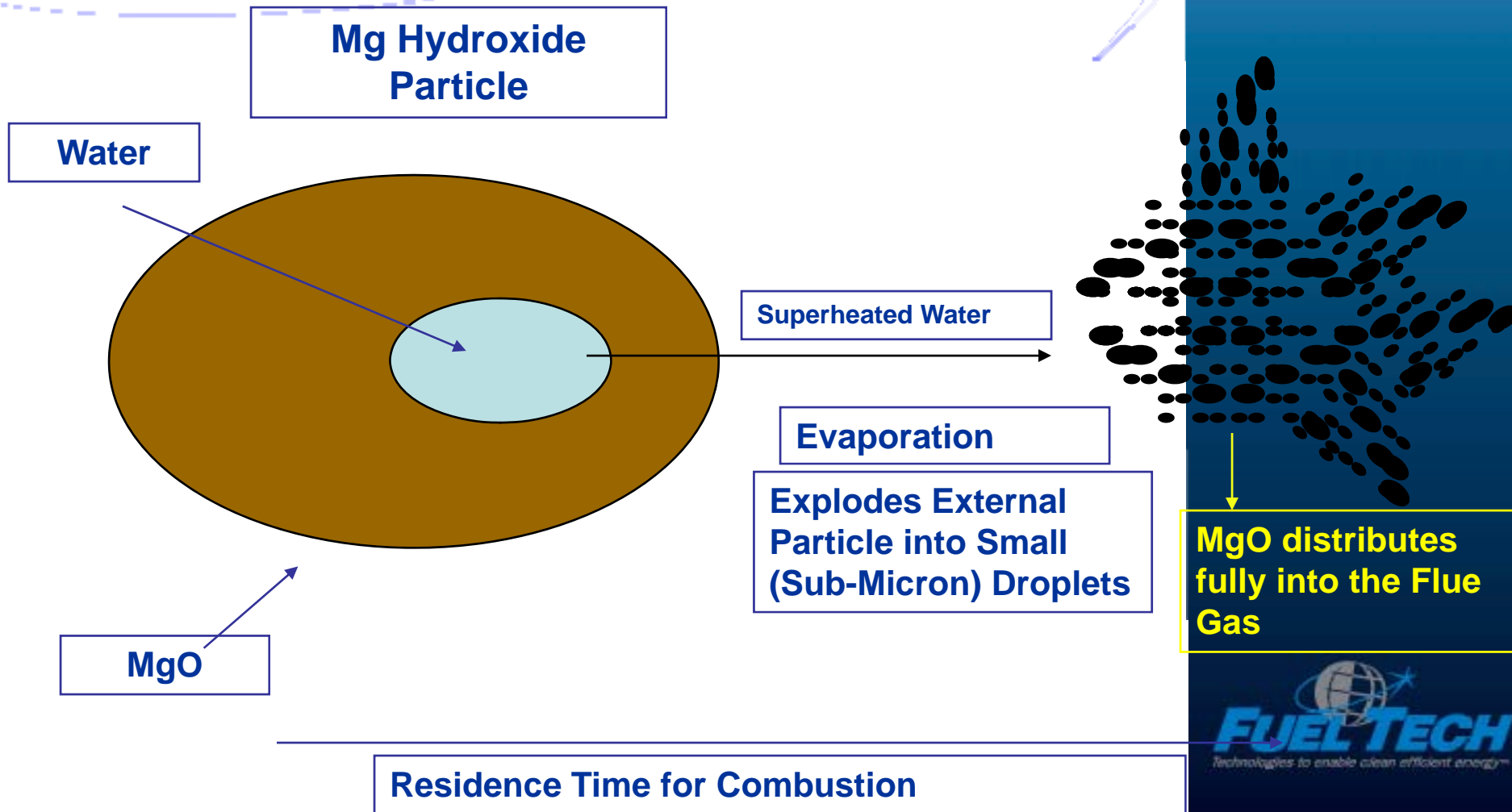
STRUCTURE

- NEAT / TIGHT

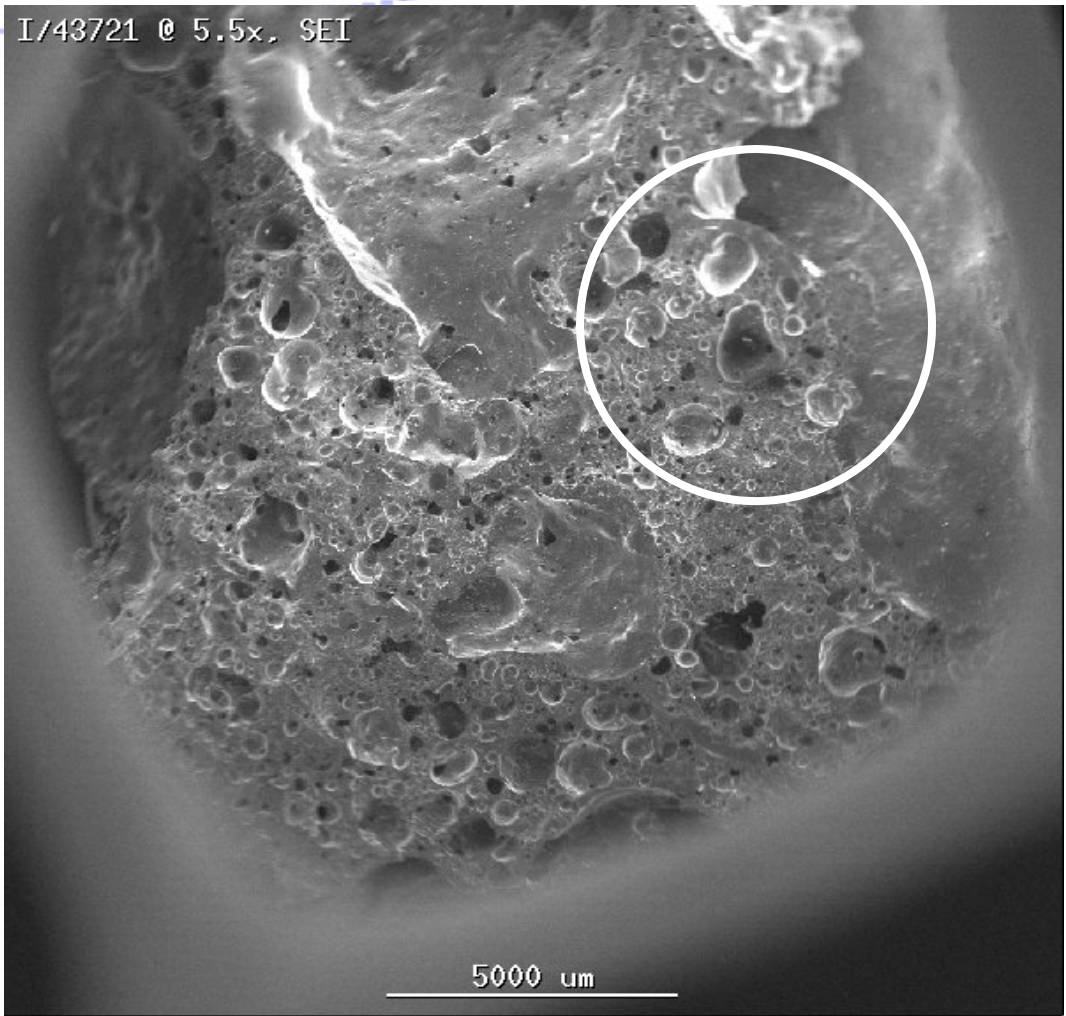
$Mg(OH)_2$:
CRYSTAL MOD
DESTROYS PACK



To Change The Deposit Morphology, The Mg Must Get INTO The Deposit

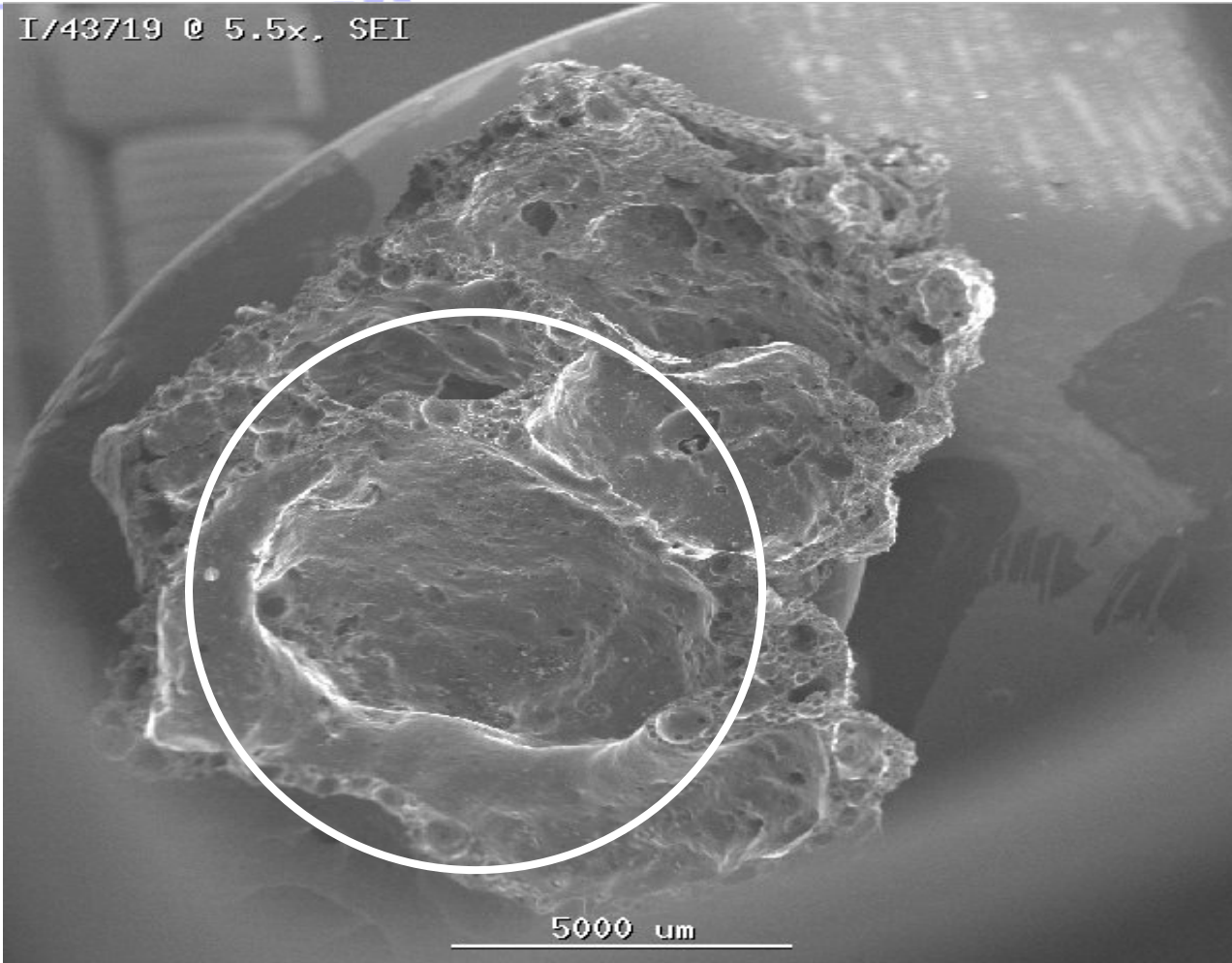


UNTREATED BASELINE SLAG WESTERN COAL FIRED (SEM 5.5x)



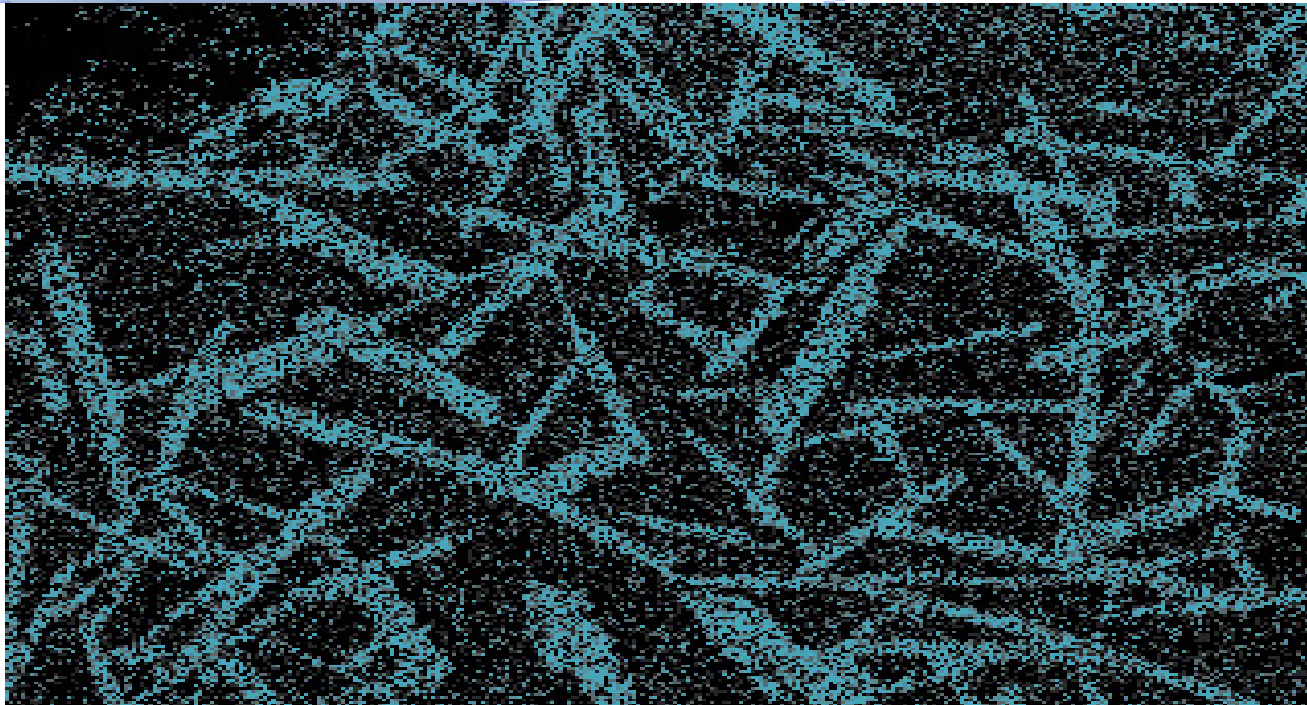
TIFI TREATED SLAG WESTERN COAL FIRED (SEM 5.5x)

I/43719 @ 5.5x, SEI



SLAG STRUCTURAL STRENGTH

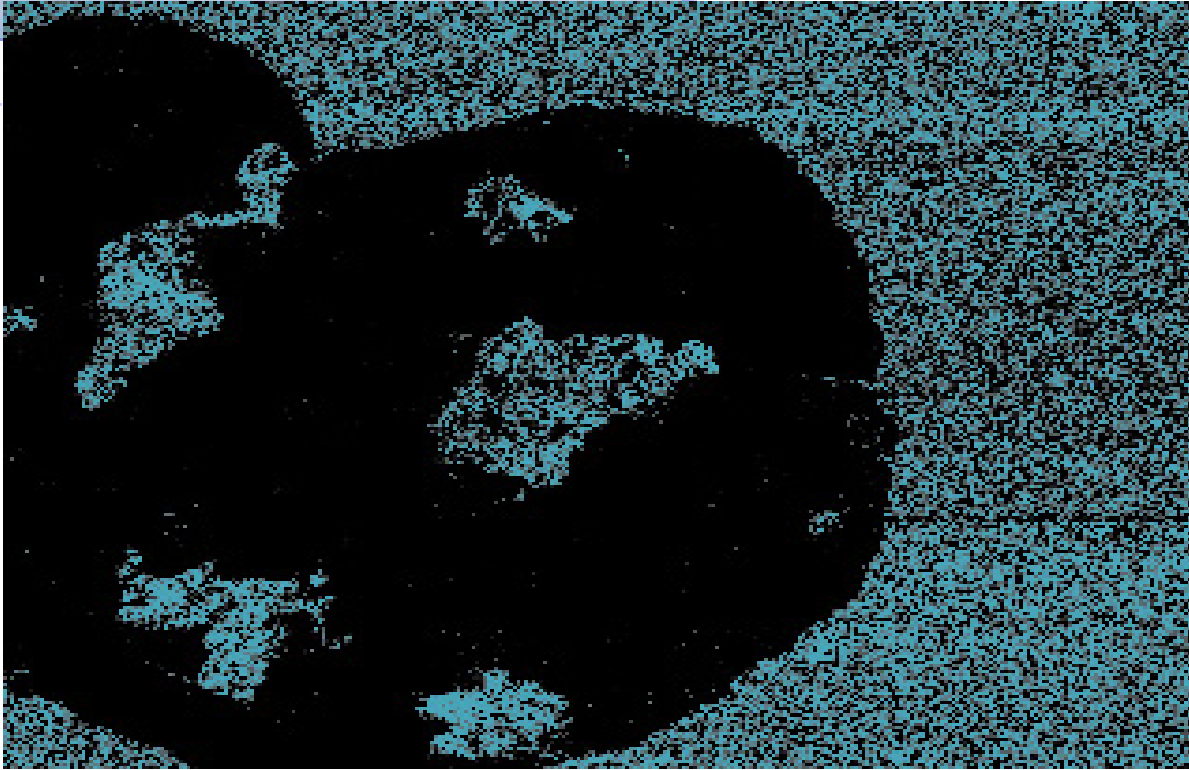
GDMS 113x Magnification Untreated



- Aluminum Color Enhanced Blue
- AL “Fibers” Add Strength
- Acts like rebar

SLAG STRUCTURAL CHANGE

GDMS 113x Magnification Treated



- Aluminum Color Enhance Blue
- AL Evenly Dispersed
- TIFI Interferes With AL Fiber Formation
- Strength & Support Lower > 50%

Illinois Basin Coal



Slag Transformation: Results of a Mid West Utility



Consistency Prior to Chemical feed



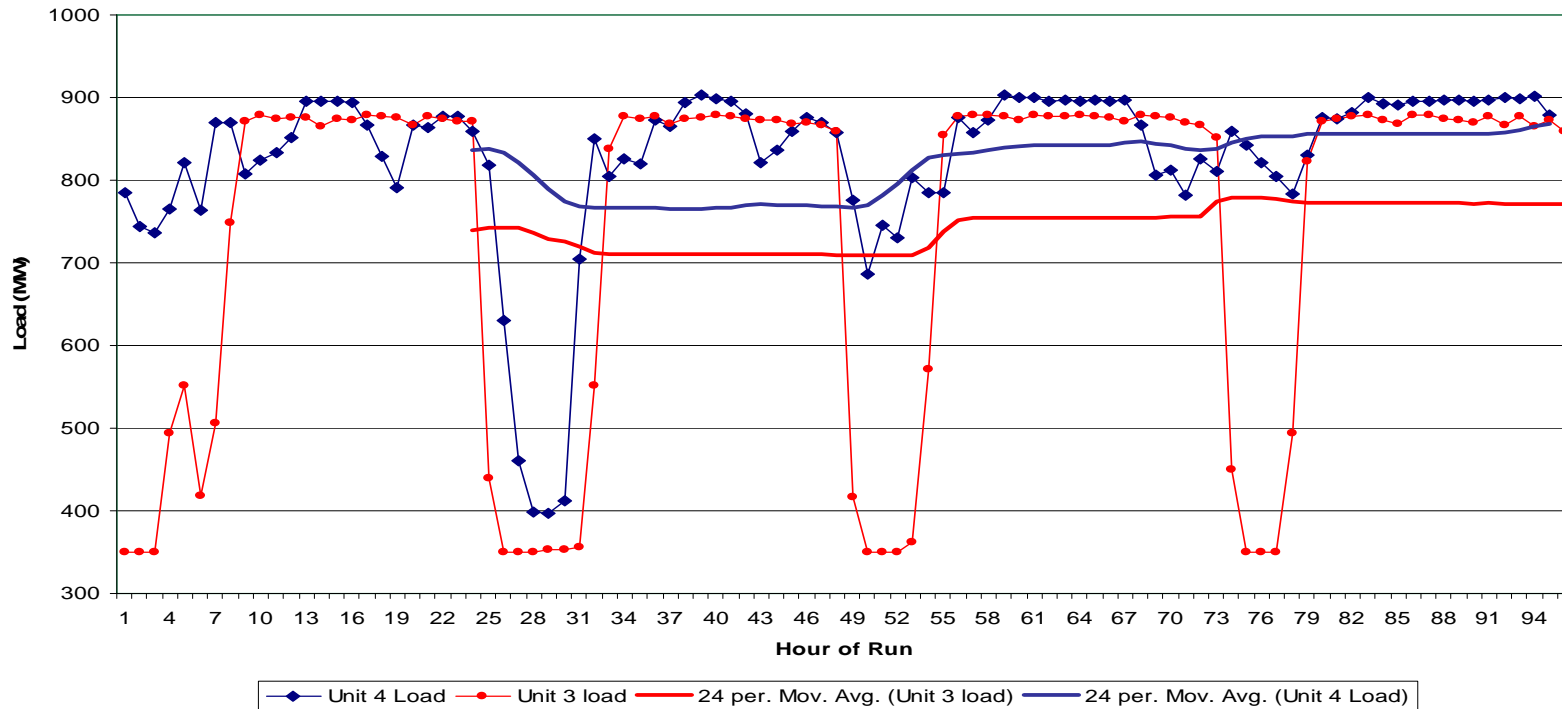
Consistency After Chemical feed

Georgia Power Scherer Program Benefits

- Soot blowing Reduction
- Recovery of Lost Megawatts
- Reduced Fireside Cleanings
- Improved Heat Rate
- Coal Price Premium
- Reduced Tube Replacement Costs
from Corrosion and Erosion

UNIT 3 vs. UNIT 4 AVG MW

Twin 900 MW Units

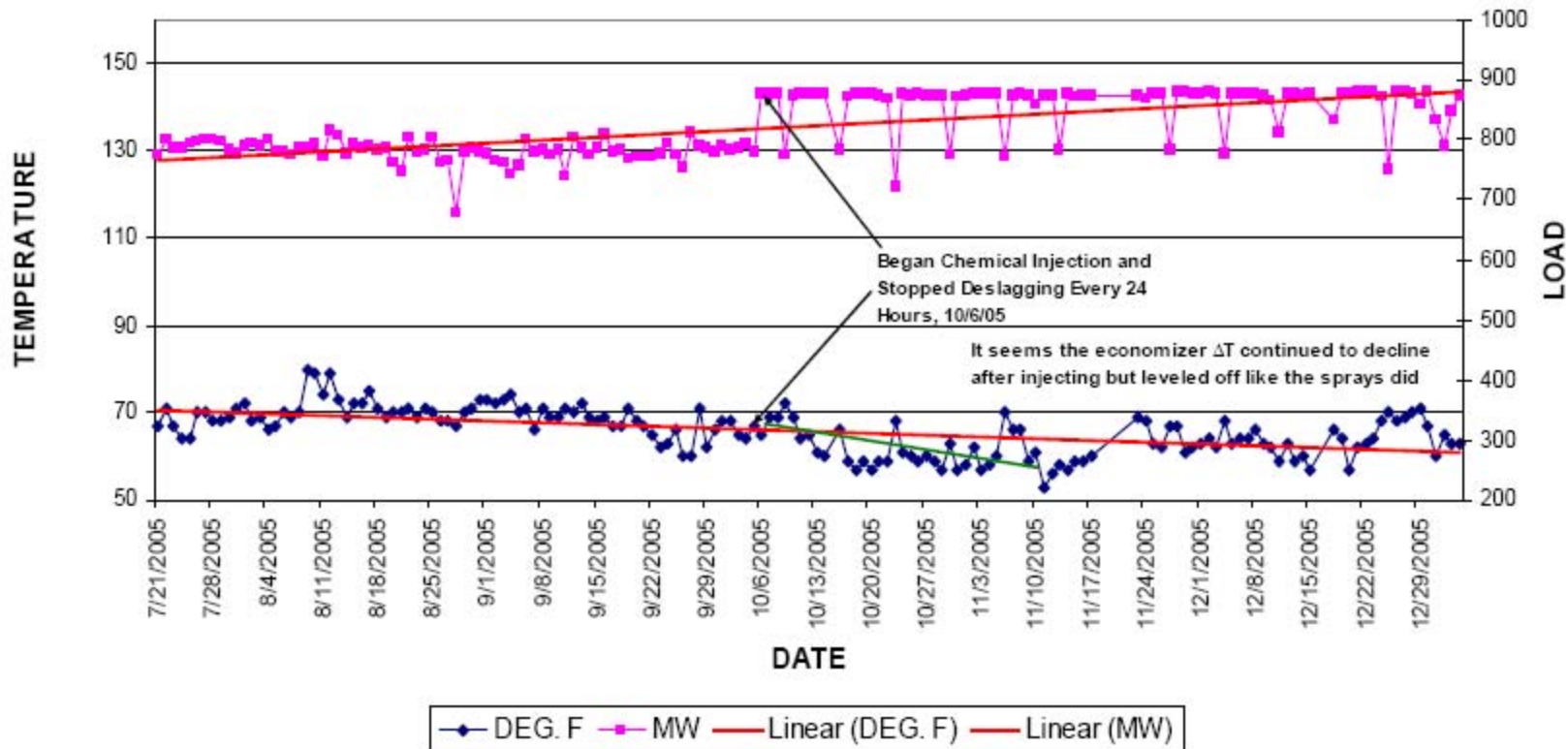


- IDENTICAL 900 MW UNITS ON PRB
- NIGHTLY DERATES DUE TO SLAG
- UNIT 3 BASELINE; UNIT 4 TIFI TREATED
- UNIT 3 HAS TO CONTINUE NIGHTLY DERATES
- UNIT 4 ABLE TO AVERAGE 80 – 100 MW MORE

Decrease in Reheat Spray Flows



Increase in MW production

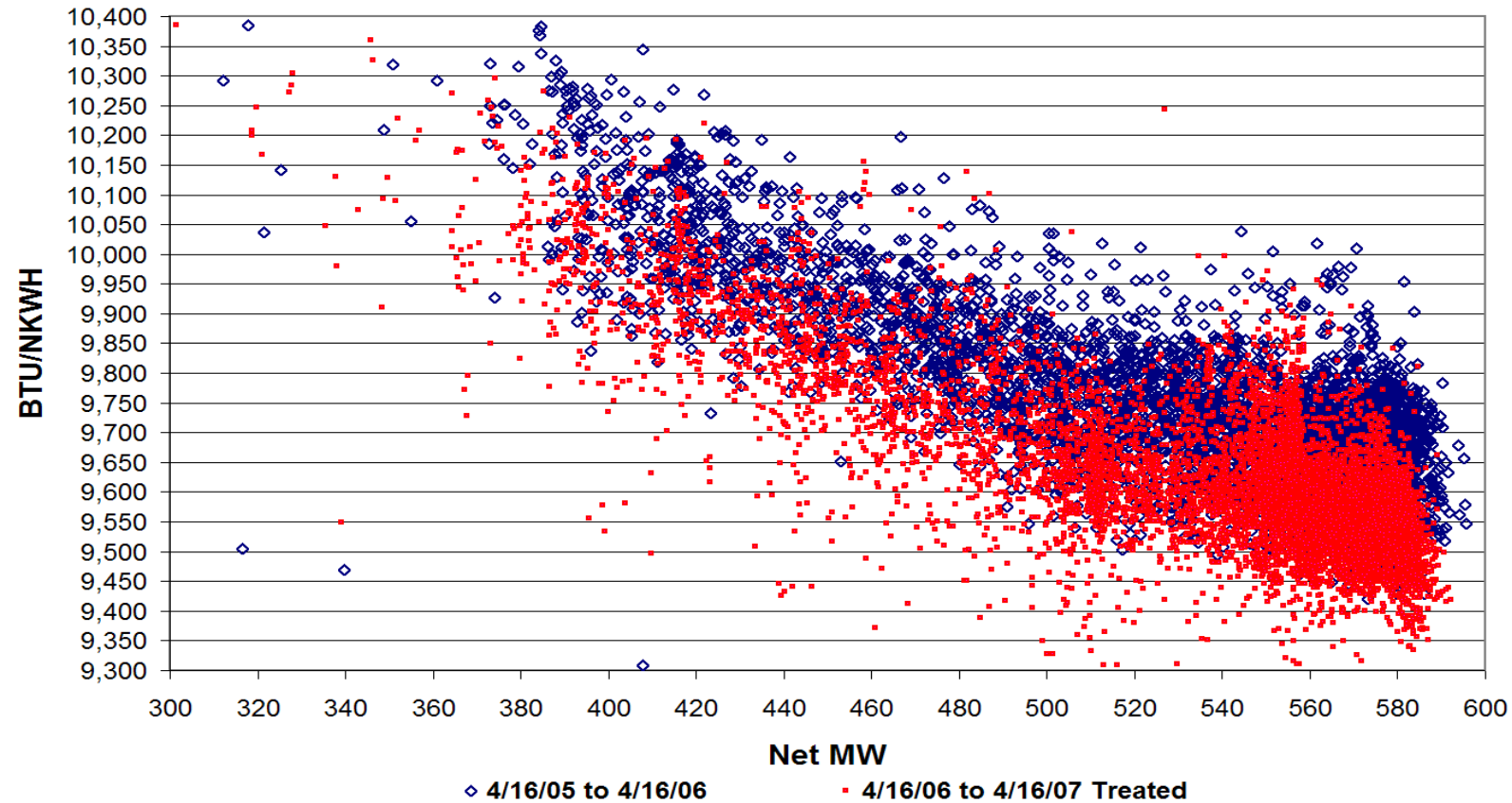


Santee Cooper Program Benefit Highlights

- ❑ Removal of SO₃ related Opacity
- ❑ 44.5 MW Increase
- ❑ Boiler Efficiency Increase of 0.65%
- ❑ 120 BTU/KW-h Heat Rate Improvement while burning coals with average heat content DECREASE of 225 BTU/lb
- ❑ 20% TTR Reduction
- ❑ 50% Outage Cleaning Time Reduction
- ❑ Mitigation of LPA
- ❑ **Greater than 4:1 Annual Return**

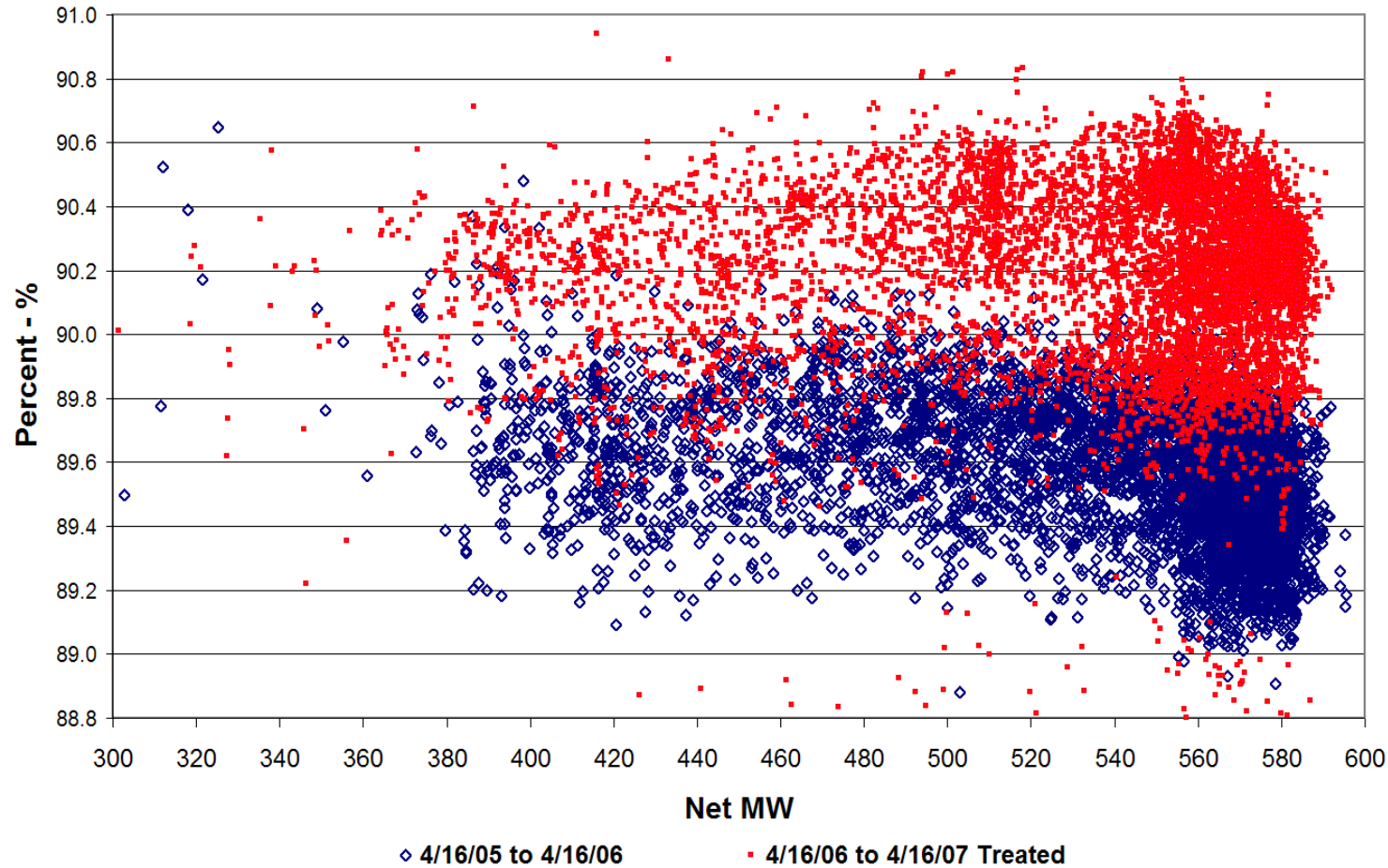
Heat Rate Improvement

Net Heat Rate Comparison



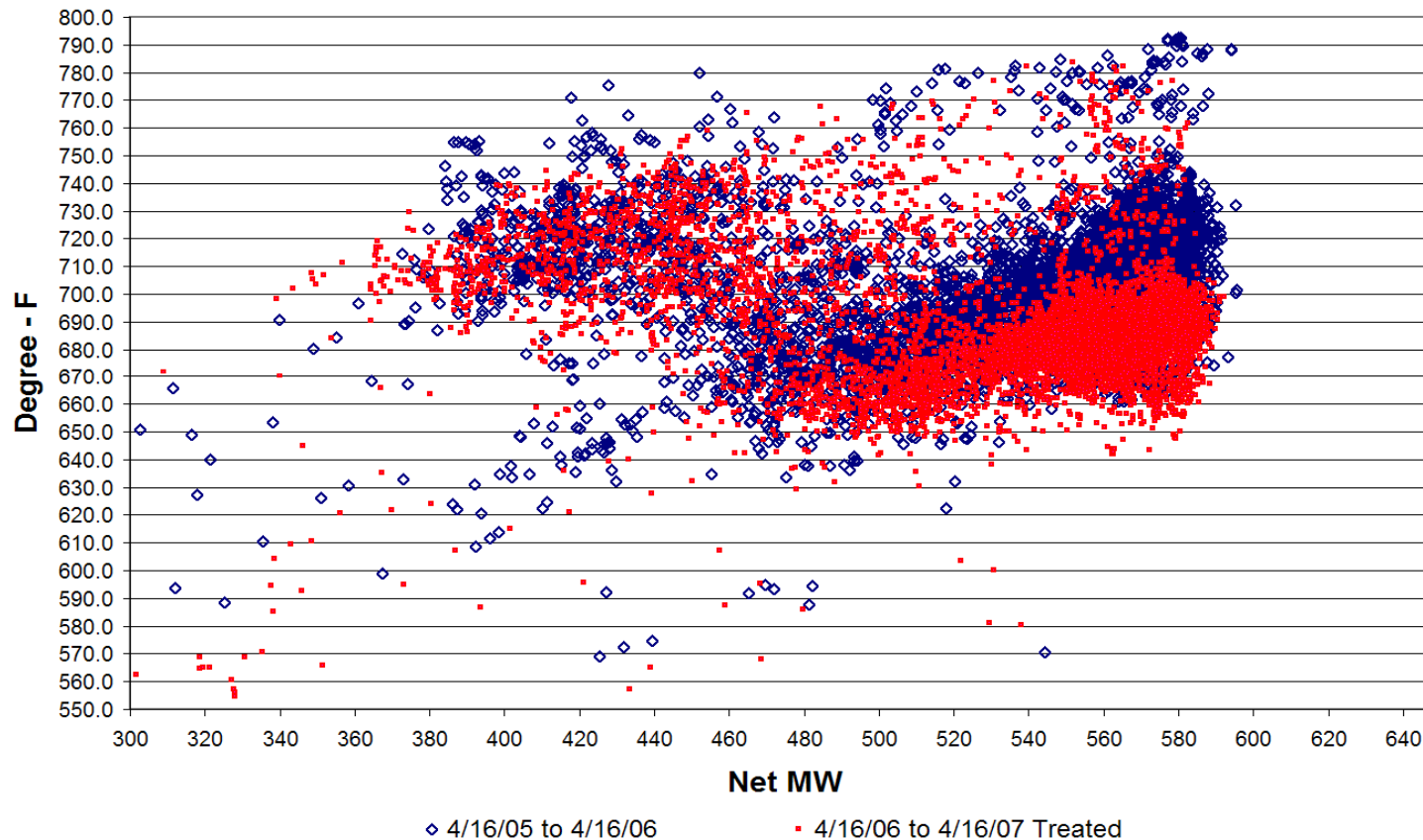
Boiler Efficiency Improvement

Boiler Efficiency Comparison



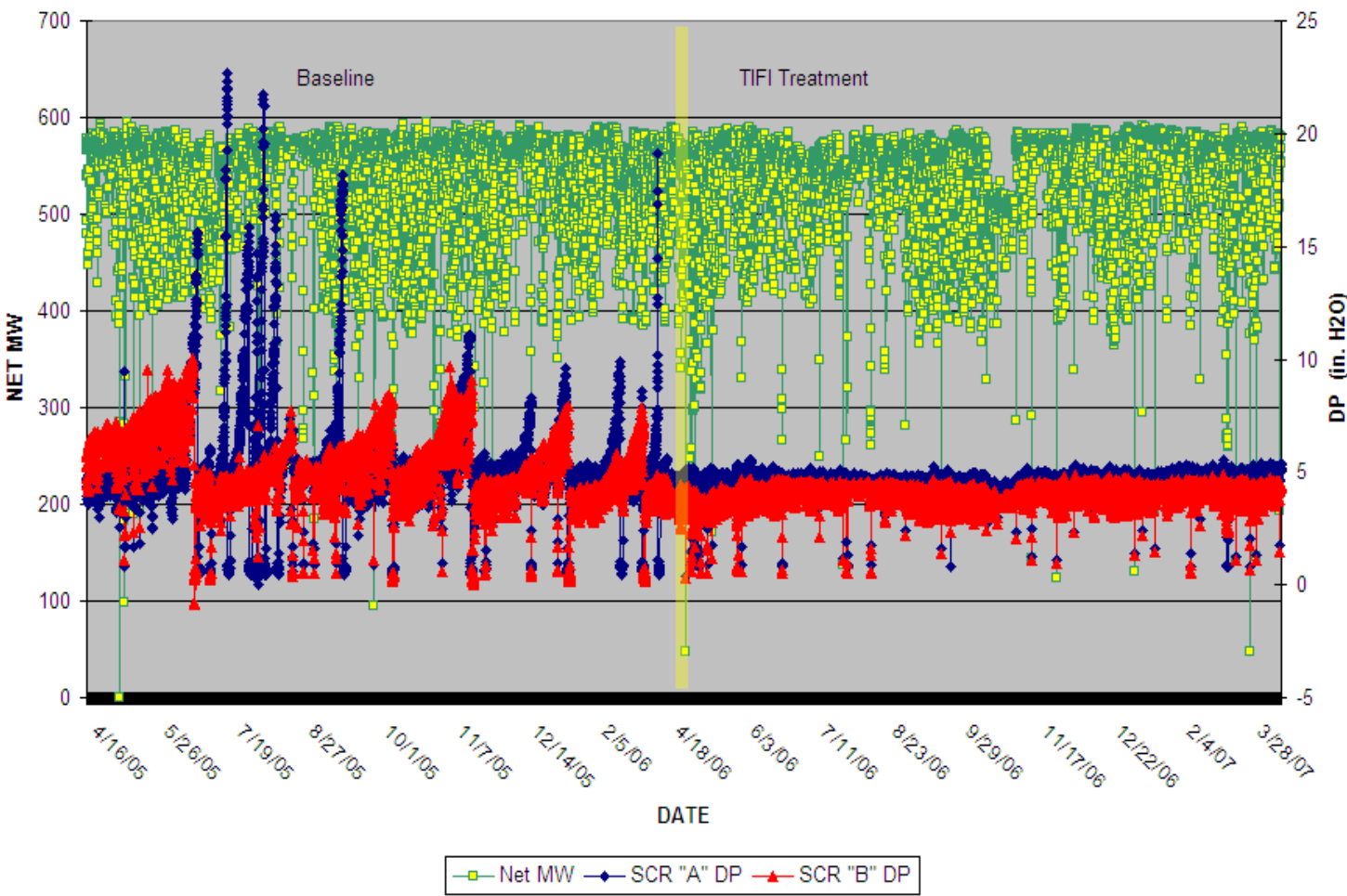
Air Heater Inlet Temps

Air Heater A Averaged Inlet Gas Temperature



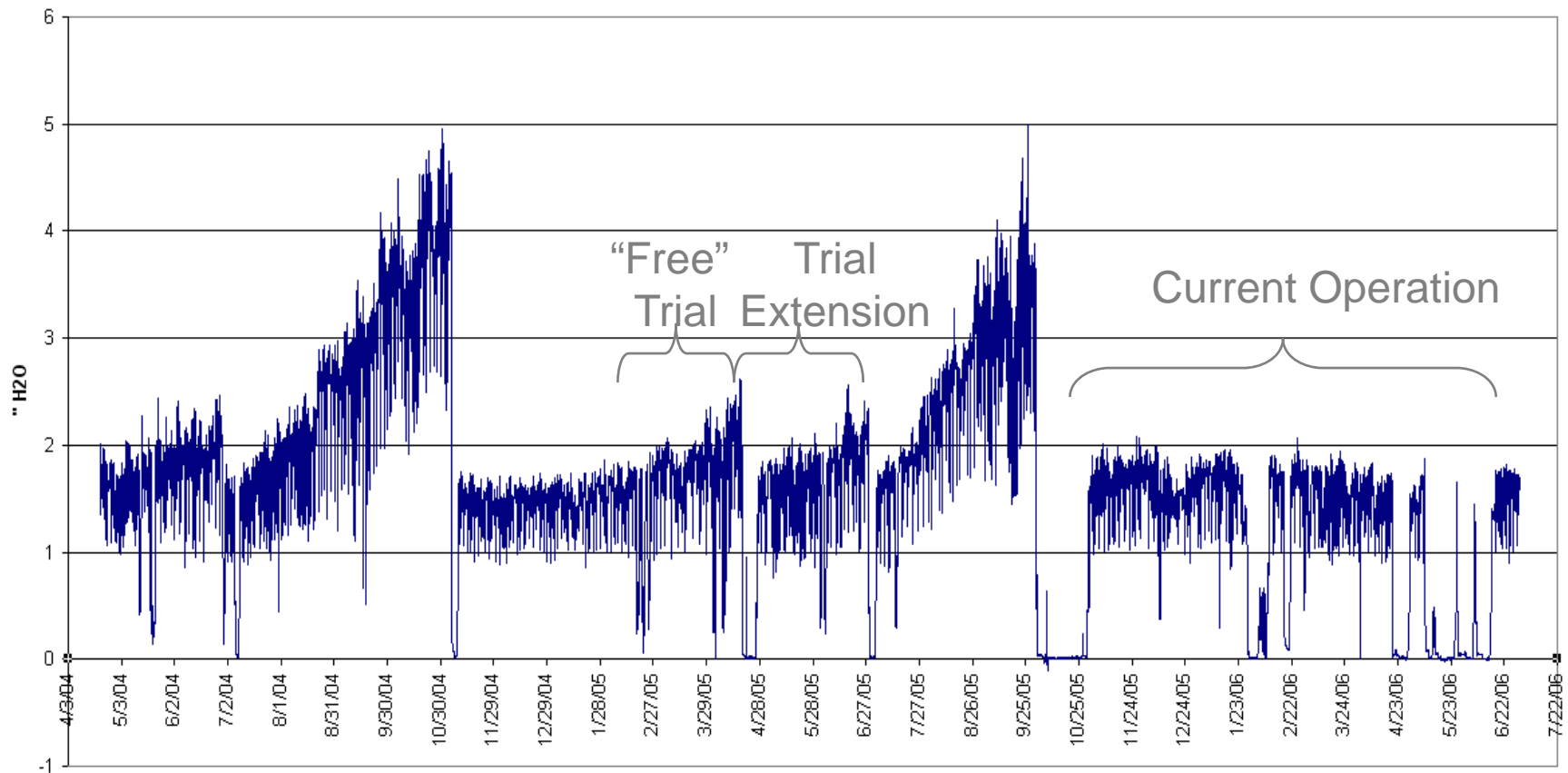
Reduction of Popcorn Ash Fouling

NET MW vs. SCR DP



MidSize Unit

REHEAT DIFFERENTIAL PRESSURE



WFEC Hugo Station Program Highlights

- ❑ 2.5% Capacity Factor Increase
- ❑ FEGT Drop from 2600 to 2500 F
- ❑ Excess O₂ Drop from 3.0 to 2.5
- ❑ \$500K Annual in NOx Credits
- ❑ Coal Purchase Flexibility
- ❑ 80% Outage Cleaning Time Reduction
- ❑ **3:1 Average Annual Return**

Minimize Outage Cleaning Time Requirement & Intensity



With FUEL CHEM:
12-18 hours of off-line
moderate charge
cleaning

Without FUEL CHEM:
3-5 days of off-line high
explosive cleaning

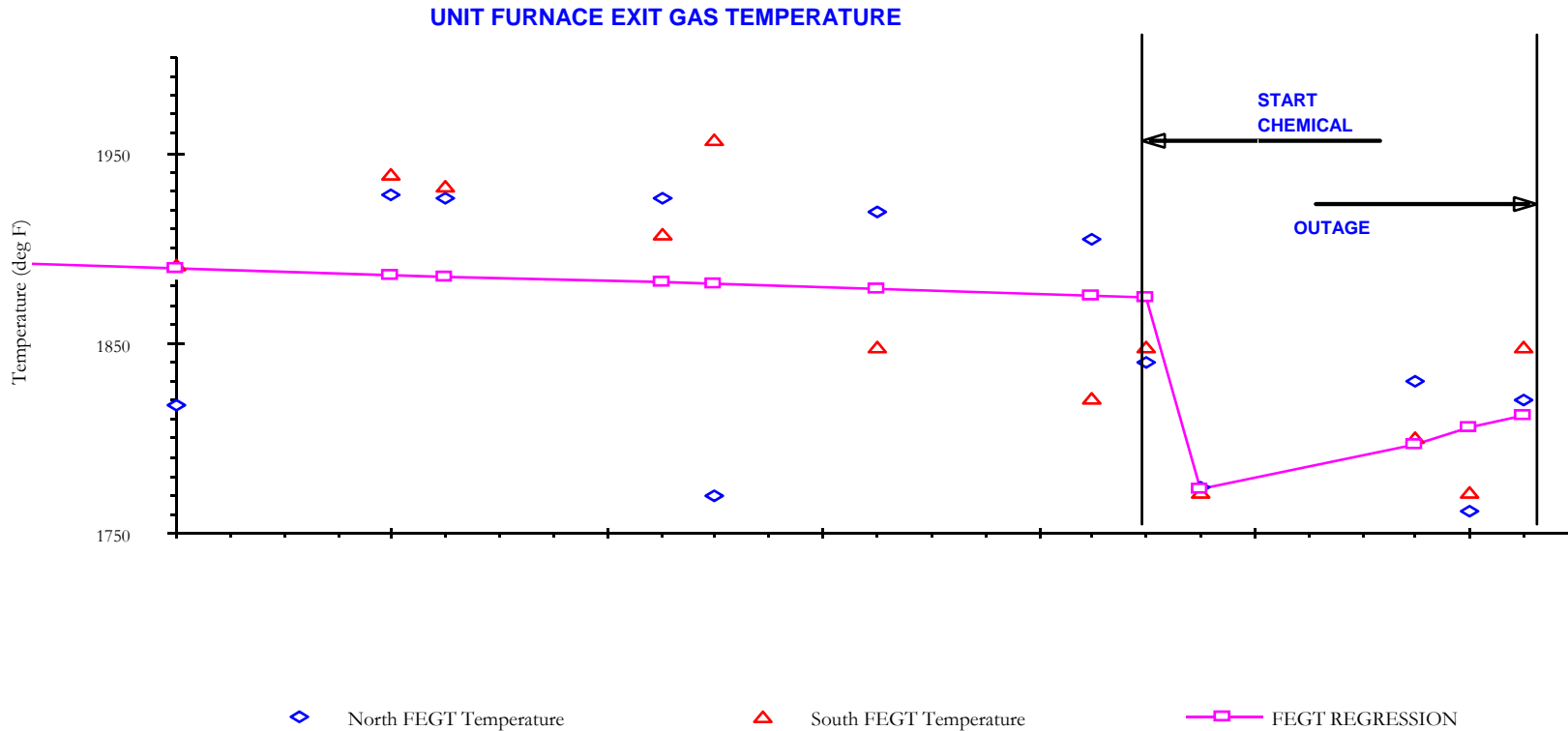


Transalta Program Benefit Highlights

- ❑ Cleaning outage avoidance of 10 days/unit/year
- ❑ Cleaning cost avoidance ~ \$100,000/day
- ❑ Increased generation capacity – derate reduction
- ❑ Economizer cleanliness = ~ 30 MW gain
- ❑ Bottom ash maintenance improvement – grinders, no issues, no clinkers
- ❑ Fuel flexibility – Spring Creek and Rawhide
- ❑ **4:1 Average Annual Return**

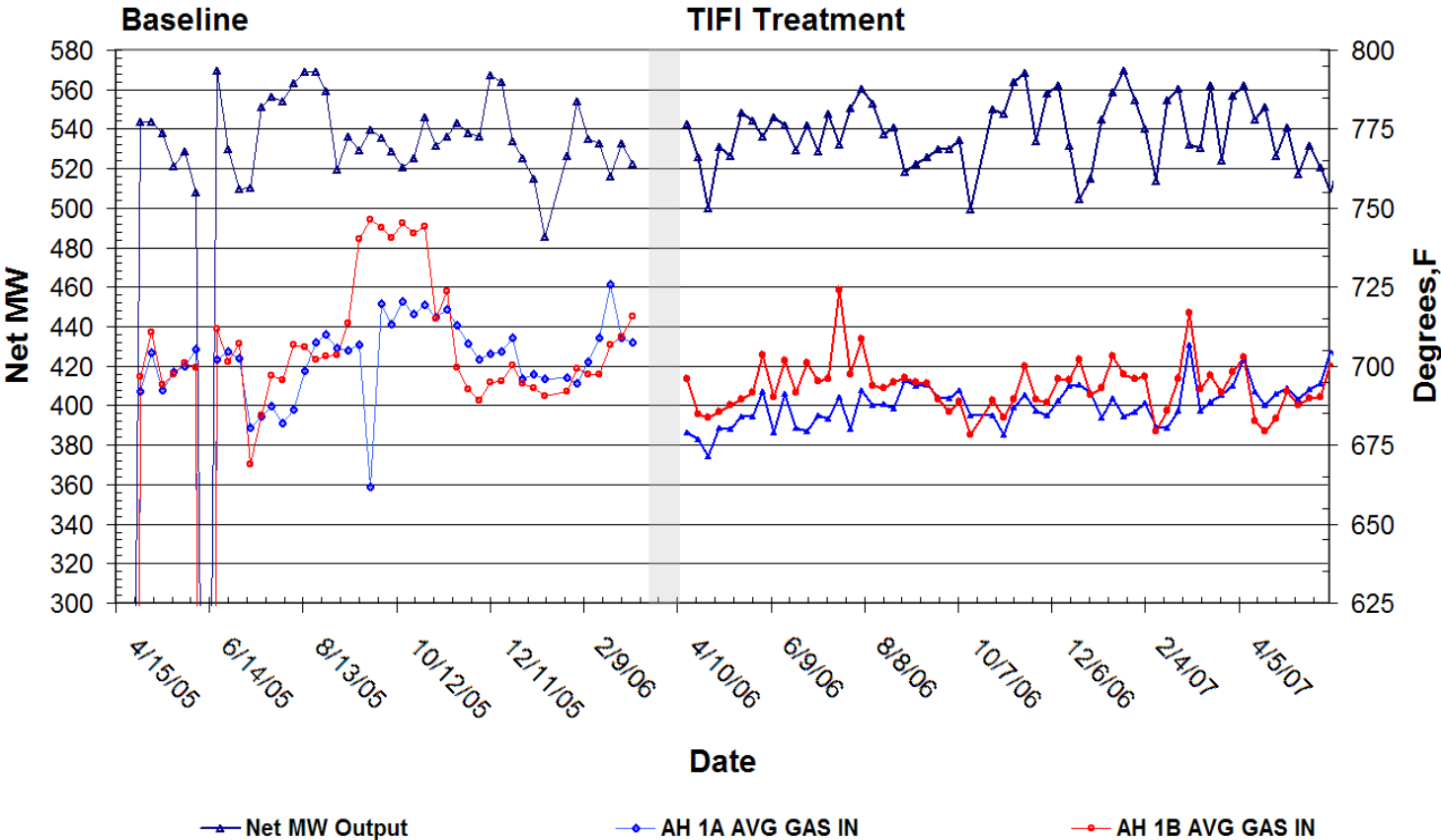
Midwestern Utility

- Started on a dirty boiler
- Prior to start, Unit was restricted due to high steam temps
- Capacity increased and visual clean up occurred.
- Ability to keep Steam Temps below 1000F



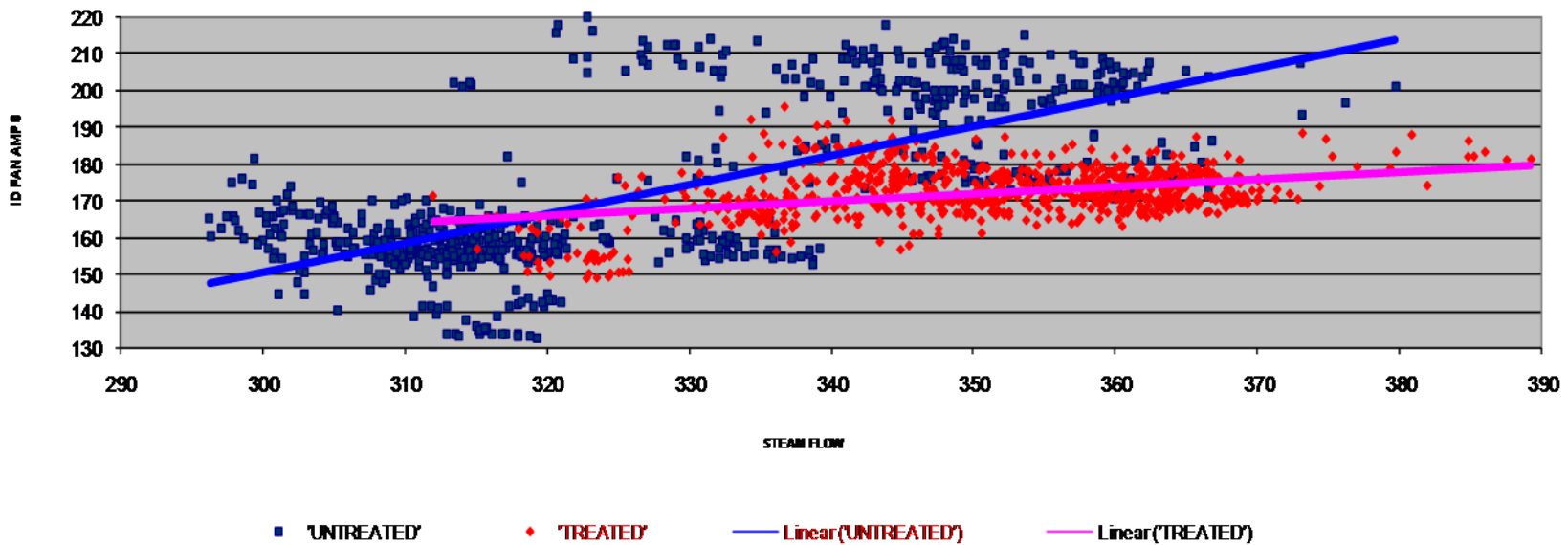
Peak Generation Increase

Net Generation MW & Weekly Average AH Inlet Gas Temperature

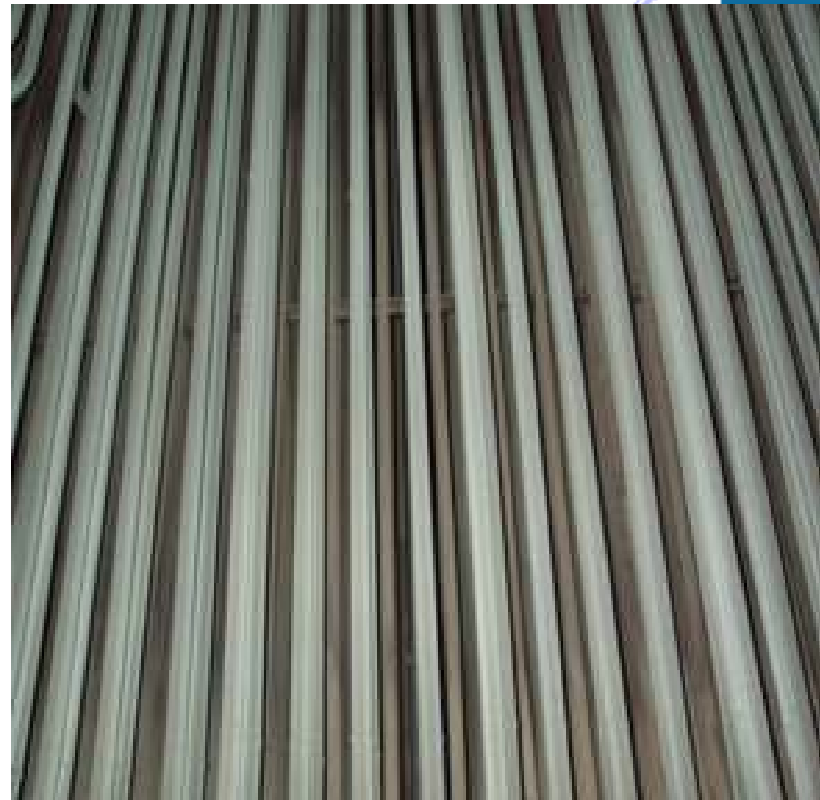


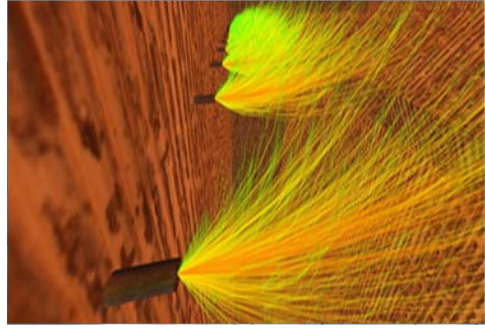
Midwestern Industrial

ID FAN AMPS VS STEAM FLOW



Midwestern Utility





Questions